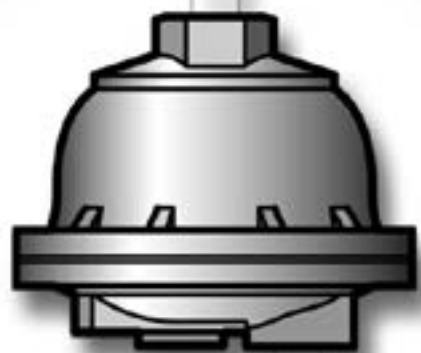


Liquid Drainers



Armstrong





32-LD Forged Steel Free Floating
Lever Drain Trap



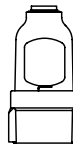
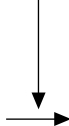
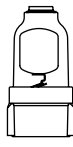
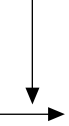
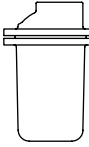
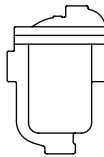
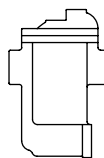
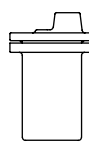
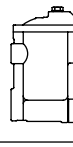
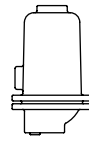
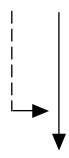
1-LD Cast Iron Free Floating
Lever Drain Trap



11-LD Stainless Steel Free Floating
Lever Drain Trap

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Liquid Drainers ID Charts

Armstrong Liquid Drainers															
Illustration	Type	Flow Direction	Connection Type	Max. Allow. Press. psig	TMA °F	Body Material	Model	Max. Oper. Press. psig	Connection Size						Located on Page
									1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	
	Series 1-LDC See-Thru Free Floating Lever Drain Traps Capacities to 1 500 lb/hr		Screwed	150	150	Nylon Cap Polycarbonate Body	1-LDC	150	●	★ ★ ●					535
	Series 1-LDCW See-Thru Free Floating Lever Drain Traps for Ozone Applications Capacities to 1 500 lb/hr		Screwed	150	150	PBT Cap (Polybutylene Terephthalate) Polycarbonate Body	1-LDCW		▲	★ ★ ●					536
	Series 200 BVSU Inverted Bucket Drain Traps Capacities to 7 000 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	211 212 213	250	● ● ●	● ● ●	●				538
	Series 800 BVSU Inverted Bucket Drain Traps Capacities to 7 000 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	800 811 812 813	150 250 250 250	● ● ● ●	● ● ● ●	● ● ●				537
	Series 880 BVSU Inverted Bucket Drain Traps Capacities to 7 000 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	880 881 882 883	150 250 250 250	● ● ● ●	● ● ● ●	● ● ●				537
	Series 300 BVSU Inverted Bucket Drain Traps Capacities to 7 000 lb/hr		Screwed Socketweld Flanged†	600 1 080	650 650	ASTM A105 Forged Steel	312 313	600	● ●	● ●	● ●				537
	Series 900 BVSU Inverted Bucket Drain Traps Capacities to 7 000 lb/hr		Screwed Socketweld Flanged†	600	650	ASTM A216 WCB Cast Steel	971 973	300 600	● ●	● ●	● ●				537
	Series 1, 2, 3, 6 Free Floating Lever Drain Traps Capacities to 49 000 lb/hr		Screwed	300 250	200 450	ASTM A48 Class 30 Cast Iron	1-LD 2-LD 3-LD 6-LD	300 250	★ ● ● ●	● ● ● ●	● ●			● ●	540

★ 1/4" outlet connection

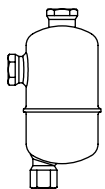
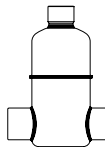
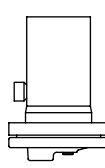
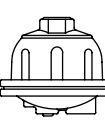
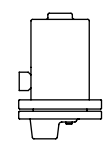
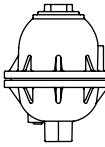
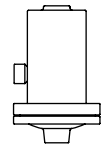
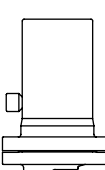
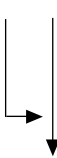
★★ 1/2" outlet connection

† Flange selection may limit pressure and temperature rating.

†† Side connection not available.

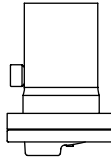
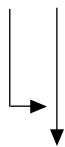
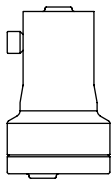
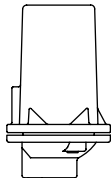
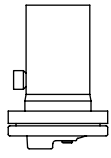
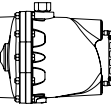
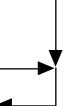
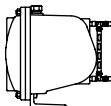
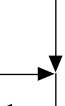
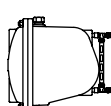


Armstrong® Liquid Drainers ID Charts

Armstrong Liquid Drainers															
Illustration	Type	Flow Direction	Connection Type	Max. Allow. Press. psig	TMA °F	Body Material	Model	Max. Oper. Press. psig	Connection Size						Located on Page
									1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	
	Series 11, 22, 13 Free Floating Lever Drain Traps		Screwed Socketweld	500 or 440	100 or 500	304-L Stainless Steel	11-LD^{††}	400	●	★★ ●					541
	Screwed Socketweld (22 and 13 Series Only)		600 or 475	100 or 500	22-LD		533		●						
			570 or 490	100 or 500	13-LD		570			●					
	180-LD/181-LD Free Floating Lever Drain Traps		Screwed Socketweld	500 or 440	100 or 500	304L Stainless Steel	180-LD	229	●						543
	181-LD						350		●						
	Series 30 Free Floating Lever Drain Traps		Screwed Socketweld Flanged [†]	600 or 500	100 or 750	ASTM A105 Forged Steel	32-LD	600	●	●	●				542
	1 000 or 600			100 or 750	33-LD		900	●	●	●					
	1 000 or 600			100 or 750	36-LD		1 000					●	●		
	Series 21 Fixed Pivot Drain Trap		Screwed	250	450	ASTM A48 Class 30 Cast Iron	21	250	●	●					545
	Series 21-312 Fixed Pivot Drain Traps		Screwed Socketweld Flanged [†]	600 or 500	100 or 750	ASTM A105 Forged Steel	21-312	74	●	●	●				
	21-312V						600	●	●	●					
	Series 71-A Snap Action Drain Trap		Screwed	250	450	ASTM A48 Class 30 Cast Iron	71-A	250		●	●				
	Series 71-315 Snap Action Drain Trap		Screwed Socketweld Flanged [†]	1 000 or 600	100 or 750	ASTM A105 Forged Steel	71-315	1 000		●	●	●			
	Series 2300 High Leverage Spring-Loaded Float Type Drain Trap		Screwed Socketweld Flanged [†]	1 000 or 600	100 or 750	ASTM A105 Forged Steel	2313-HLS	1 000	●	●	●				547
Capacities to 14 500 lb/hr									●	●	●				

[†] Flange selection may limit pressure and temperature rating.

Liquid Drainers ID Charts

Armstrong Liquid Drainers																	
Illustration	Type	Flow Direction	Connection Type	Max. Allow. Press. psig	TMA °F	Body Material	Model	Max. Oper. Press. psig	Connection Size								Located on Page
									1/2"	3/4"	1"	1-1/4"	1-1/2"	2"	2-1/2"	3"	
	Series 2400 High Leverage Spring-Loaded Float Type Drain Traps Capacities to 16 250 lb/hr		Screwed Socketweld Flanged†	1 500 or 900	100 or 850	ASTM A182 Gr. F22 Forged Steel	2413-HLS	1 500	●	●	●						547
				1 800 or 900	100 or 900		2415-HLS	1 800			●	●	●			547	
							2416-HLS	1 800				●	●				
	Series 2500/2600 High Leverage Spring-Loaded Float Type Drain Traps Capacities to 11 000 lb/hr		Screwed Socketweld Flanged†	2 120 or 1 700	100 or 900	ASTM A182 Gr. F22 Forged Steel	25133G HLS	2 120		●	●	●					547
				2 520 or 2 000	100 or 900		25155G HLS	2 520			●	●	●				
				3 700 or 3 000	100 or 900		26155G HLS	3 700				●	●				
	Series 2, 3, 6 Free Floating Lever Dual Gravity Drain Traps Capacities to 40 000 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	2-DG	190	●	●							549
							3-DG	250		●	●						
							6-DG	250				●	●				
	Series 30 Free Floating Lever Dual Gravity Drain Traps Capacities to 40 000 lb/hr		Screwed Socketweld Flanged†	600 or 500	100 or 750	ASTM A105 Forged Steel	32-DG	325	●	●	●						549
				1 000 or 600	100 or 750		33-DG	700		●	●						
				1 000 or 600	100 or 750		36-DG	1 000				●	●				
	Series JD&KD Ultra-Capacity Drain Traps Capacities to 302 000 lb/hr		Screwed	300	650	ASTM A395 Ductile Iron	JD8 KD8 KD10 KD12	300*						●	●	●	551
	Series L&M Ultra-Capacity Drain Traps Capacities to 700 000 lb/hr		Screwed	250	450	ASTM A48 Class 30 Cast Iron	L8 L10 M12	250*						●		●	
	Series LS&MS Ultra-Capacity Drain Traps Capacities to 700 000 lb/hr		Screwed Socketweld Flanged†	450	650	ASTM A216 WCB Cast Steel	LS8 LS10 MS12	450*						●		●	

*For different specific gravities, see table LD-33 on page LD-49.

†Flange selection may limit pressure and temperature rating.



Armstrong® Bringing Energy Down to Earth

Say energy. Think environment. And vice versa.

Any company that is energy conscious is also environmentally conscious. Less energy consumed means less waste, fewer emissions and a healthier environment.

In short, bringing energy and environment together lowers the cost industry must pay for both. By helping companies manage energy, Armstrong products and services are also helping to protect the environment.

Armstrong has been sharing know-how since we invented the energy-efficient inverted bucket steam trap in 1911. In the years since, customers' savings have proven again and again that knowledge not shared is energy wasted.

Armstrong's developments and improvements in drain trap design and function have led to countless savings in energy, time and money. This section has grown out of our decades of sharing and expanding what we've learned. It deals with the operating principles of drain traps and outlines their specific applications to a wide variety of products and industries.

This section also includes Recommendation Charts that summarize our findings on which type of drain trap will give optimum performance in a given situation and why.

Terminology

Drain traps, as described in this section, have many other names in industry. A drain trap is an automatic loss prevention valve that opens to discharge liquids and closes to prevent air or gas loss. In industry, drain traps are also known as:

- | | |
|-------------------------|------------------------|
| ■ Compressed air drains | ■ Dump valves |
| ■ Condensate drainers | ■ Float traps |
| ■ Air traps | ■ Liquid drainers |
| ■ Water traps | ■ Compressed air traps |

This section should be utilized as a guide for the installation and operation of drain trapping equipment by experienced personnel. Selection or installation should always be accompanied by competent technical assistance or advice. We encourage you to contact Armstrong or its local representative for complete details.

Instructions for Using the Recommendation Charts



Quick reference Recommendation Charts appear throughout the “HOW TO DRAIN” pages of this section, pages LD-17 to LD-28.

A feature code system (ranging from A to N) supplies you with “at-a-glance” information.

The chart covers the type of drain traps and the major advantages that Armstrong feels are superior for each particular application.

For example, assume you are looking for information concerning the proper trap to use on an aftercooler. You would:

1. Turn to the “How to Drain Aftercoolers” section, pages LD-21 and LD-22, and look in the lower left-hand corner of page LD-21. (Each application has a Recommendation Chart.) The Recommendation Chart LD-7 from page LD-21 is reprinted below as Chart LD-1 for your convenience.

2. Find “Aftercooler” in the first column under “Equipment Being Drained” and read to the right for Armstrong’s “1st Choice and Feature Code”. In this case, the first choice is an IB and the feature code letters F, G, J, K, M are listed.

3. Now refer to the chart below, titled “How Various Types of Drain Traps Meet Specific Operating Requirements” and read down the extreme left-hand column to each of the letters F, G, J, K, M. The letter “F,” for example, refers to the trap’s ability to handle oil/water mix.

4. Follow the line for “F” to the right until you reach the column that corresponds to our first choice, in this case the inverted bucket. Based on tests, actual operating conditions, and the fact that the discharge is at the top, the inverted bucket trap handles oil/water mixtures extremely well. Follow this same procedure for the remaining letters.

Chart LD-1. Recommendation Chart (See below for “Feature Code” references.)				
Equipment Being Drained	Air		Gas	
	1st Choice and Feature Code	Alternate Choice	1st Choice and Feature Code	Alternate Choice
Aftercooler	IB	FF	*FF	FP
Intercooler	F, G, J, K, M		B, E, J	

*Since IBs vent gas to operate, an FF is suggested because gas venting may not be desirable.

Chart LD-2. How Various Types of Drain Traps Meet Specific Operating Requirements								
Feature Code	Characteristic	IB	FF	FP	FS	D	TV	MV
A	Method of Operation (Intermittent-Continuous)	I	C	C	I	I	I	C
B	Energy Conservation in Operation	Good	Excellent	Excellent	Excellent	Fair	Poor	Excellent
C	Energy Conservation Over Time	Good	Excellent	Excellent	Excellent	Poor	Fair	Poor (5)
D	Resistance to Wear Fair	Excellent	Excellent	Fair	Good	Poor	Good	Excellent
E	Corrosion Resistance	Excellent	Excellent	Excellent	Excellent	Excellent	Excellent	Excellent
F	Ability to Handle Oil/Water Mix	Excellent	Fair	Fair	Fair	Good	Excellent	Excellent
G	Ability to Prevent Sludge Buildup	Excellent	Poor	Poor	Fair	Good	Good	Excellent
H	Resistance to Damage from Freezing (1)	Good (2)	Poor	Poor	Poor	Good	Fair	Good
I	Performance to Very Light Loads	Good	Excellent	Excellent	Excellent	Poor	Poor	Poor
J	Responsiveness to Slugs of Liquid (3)	Good	Excellent	Excellent	Excellent	Poor	Poor	Poor
K	Ability to Handle Dirt	Excellent	Fair	Fair	Excellent	Poor	Excellent	Good
L	Comparative Physical Size	Large	Large	Large	Large	Small	Small	Small
M	Mechanical Failure (Open-Closed)	Open	Closed	Closed	Closed	Open	(4)	(4)
N	Noise Level of Discharge (Loud-Quiet)	Quiet	Quiet	Quiet	Quiet	Loud	Loud	(4)

IB = Inverted Bucket
 FF = Float-Free Linkage
 FP = Float-Fixed Pivot Linkage
 FS = Float-Snap Acting Linkage
 D = Disc
 TV = Timed Solenoid Valve
 MV = Manual Valve

- (1) Cast iron not recommended.
- (2) Sealed stainless steel = good.
- (3) Float traps should be back vented = excellent.
- (4) Can be either.
- (5) Usually end up “cracked open.”



Compressed Air/Gases—Basic Concepts

Moisture is always present in compressed air, and oil can be present at some points in a compressed air system. For the efficient operation and long life of gaskets, hoses and air tools, this excess moisture and the oil must be removed from the system.

The removal of moisture and oil from a system involves more than just traps. To maintain high efficiency and avoid costly problems, a compressed air system also requires:

1. Aftercoolers to bring the compressed air down to ambient or room temperature.
2. Separators to knock down suspended droplets of water or fog. Separators are installed downstream from aftercoolers or in air lines near point of use, or both.
3. Drain traps to discharge the liquid from the system with a minimum loss of air.

Table LD-1. Weight of Water Per Cubic Foot of Air at Various Temperatures

Temp. °F	Percentage of Saturation									
	10	20	30	40	50	60	70	80	90	100
	Grains	Grains	Grains	Grains	Grains	Grains	Grains	Grains	Grains	Grains
-10	.028	.057	.086	.114	.142	.171	.200	.228	.256	.285
0	.048	.096	.144	.192	.240	.289	.337	.385	.433	.481
10	.078	.155	.233	.310	.388	.466	.543	.621	.698	.776
20	.124	.247	.370	.494	.618	.741	.864	.988	1.112	1.235
30	.194	.387	.580	.774	.968	1.161	1.354	1.548	1.742	1.935
32	.211	.422	.634	.845	1.056	1.268	1.479	1.690	1.902	2.113
35	.237	.473	.710	.946	1.183	1.420	1.656	1.893	2.129	2.366
40	.285	.570	.855	1.140	1.424	1.709	1.994	2.279	2.564	2.849
45	.341	.683	1.024	1.366	1.707	2.048	2.390	2.731	3.073	3.414
50	.408	.815	1.223	1.630	2.038	2.446	2.853	3.261	3.668	4.076
55	.485	.970	1.455	1.940	2.424	2.909	3.394	3.879	4.364	4.849
60	.574	1.149	1.724	2.298	2.872	3.447	4.022	4.596	5.170	5.745
62	.614	1.228	1.843	2.457	3.071	3.685	4.299	4.914	5.528	6.142
64	.656	1.313	1.969	2.625	3.282	3.938	4.594	5.250	5.907	6.563
66	.701	1.402	2.103	2.804	3.504	4.205	4.906	5.607	6.308	7.009
68	.748	1.496	2.244	2.992	3.740	4.488	5.236	5.984	6.732	7.480
70	.798	1.596	2.394	3.192	3.990	4.788	5.586	6.384	7.182	7.980
72	.851	1.702	2.552	3.403	4.254	5.105	5.956	6.806	7.657	8.508
74	.907	1.813	2.720	3.626	4.533	5.440	6.346	7.253	8.159	9.066
76	.966	1.931	2.896	3.862	4.828	5.793	6.758	7.724	8.690	9.655
78	1.028	2.055	3.083	4.111	5.138	6.166	7.194	8.222	9.249	10.277
80	1.093	2.187	3.280	4.374	5.467	6.560	7.654	8.747	9.841	10.934
82	1.163	2.325	3.488	4.650	5.813	6.976	8.138	9.301	10.463	11.625
84	1.236	2.471	3.707	4.942	6.178	7.414	8.649	9.885	11.120	12.326
86	1.313	2.625	3.938	5.251	6.564	7.877	9.189	10.502	11.814	13.137
88	1.394	2.787	4.181	5.575	6.968	8.362	9.756	11.150	12.543	13.997
90	1.479	2.958	4.437	5.916	7.395	8.874	10.353	11.832	13.311	14.780
92	1.569	3.138	4.707	6.276	7.844	9.413	10.982	12.551	14.120	15.639
94	1.663	3.327	4.990	6.654	8.317	9.980	11.644	13.307	14.971	16.624
96	1.763	3.525	5.288	7.050	8.813	10.576	12.338	14.101	15.863	17.676
98	1.867	3.734	5.601	7.468	9.336	11.203	13.070	14.937	16.804	18.661
100	1.977	3.953	5.930	7.906	9.883	11.860	13.836	15.813	17.789	19.766

Based on atmospheric pressure of 14.7 psia.

Compressed Air/Gases—Basic Concepts

Water carried with air into tools or machines where air is being used will wash away lubricating oil. This causes excess wear to motors and bearings and results in high maintenance expense. Without adequate lubrication, the tools and machines run sluggishly and their efficiency is lowered. This effect is particularly pronounced in the case of pneumatic hammers, drills, hoists and sand rammers, where the wearing surfaces are limited in size and the excessive wear creates air leakage.

Where air is used for paint spraying, enameling, food agitation and similar processes, the presence of water and/or oil cannot be tolerated, nor can particles of grit or scale.

In instrument air systems, water will tend to cling to small orifices and collect dirt, causing erratic operation or failure of sensitive devices.

Pipeline Troubles

When water accumulates at low points in the pipeline, the air-carrying capacity of the line is reduced. Eventually, airflow over the pool of water will begin to carry the water along at high velocity. This produces “water hammer” along the line, and may even carry over a slug of water into a tool. In cold weather, accumulations of water may freeze and burst pipelines.

Air’s Capacity to Hold Moisture

At atmospheric pressure (14.7 psia), 8 cu ft of air with an RH of 50% and a temperature of 70°F will contain 32 grains of moisture vapor.

When the pressure is doubled (without increasing the temperature) the volume is cut in half (4 cu ft), but there are still 32 grains of moisture. This means the relative humidity is now 100%—all the moisture in vapor form that it can handle.

Increasing the pressure to 100 psig (114.7 psia), the volume of air is further reduced to approximately 1 cu ft. This 1 cu ft of compressed air still at 70°F can hold a maximum eight grains of moisture.

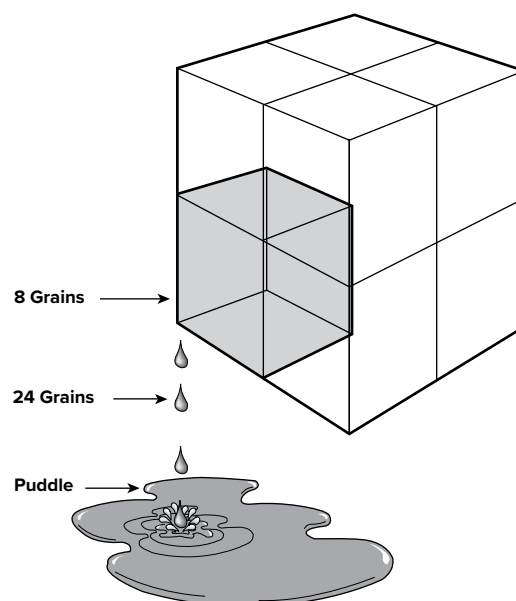
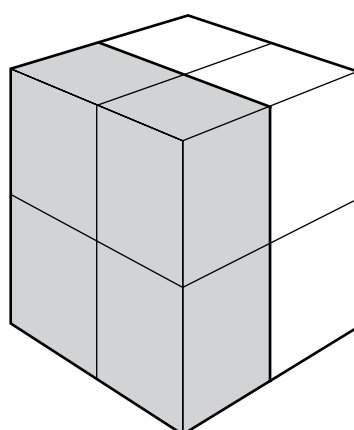
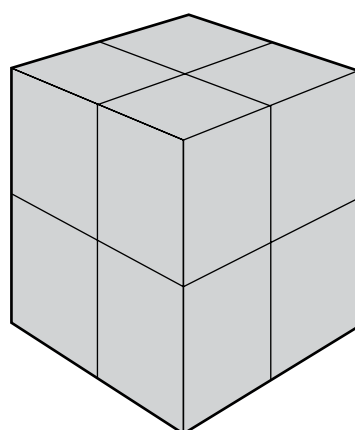


Figure LD-1.

Pressure: 0 psig (14.7 psia)
 Temp: 70°F
 Air = 8 CF
 Moisture = 32 Grains
 Max Possible = 64 Grains

Figure LD-2.

Pressure: 15 psig (29.7 psia)
 Temp: 70°F
 Air = 4 CF
 Moisture = 32 Grains
 Max Possible = 32 Grains

Figure LD-3.

Pressure: 100 psig (114.7 psia)
 Temp: 70°F
 Air = 1 CF
 Moisture = 32 Grains
 Max Possible = 8 Grains
 24 Grains of Liquid

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Drainage Problems and How to Avoid Them

Oil. A critical drainage problem exists at points where oil may be present in the compressed air (principally at intercoolers, aftercoolers and receivers).

Two facts create this problem:

1. Oil is lighter than water and will float on top of water.
2. Compressor oil when cooled tends to become thick and viscous.

The beaker simulates any drain trap that has its discharge valve at the bottom, Fig. LD-4. Like the beaker, the trap will fill with heavy oil that may be thick and viscous.

Compare with Fig. LD-5, which shows an identical beaker except that the discharge valve is at the same level as the oil. Oil will escape until the oil level is so thin that for every 19 drops of water and one of oil that enter the beaker, exactly 19 drops of water and one drop of oil will leave. The beaker always will be filled with water.

The conclusion is obvious. When there is an oil-water mixture to be drained from an air separator or receiver, use a trap with the discharge valve at the top.

Dirt and Grit. While scale and sediment is seldom a problem between the compressor and receiver, it is encountered in the air distribution system, particularly when the piping is old. In this situation, scale will be carried to a drain trap along with the water. If the drain trap is not designed to handle dirt and grit, the trap may fail to drain water and oil, or the trap valve may not close.

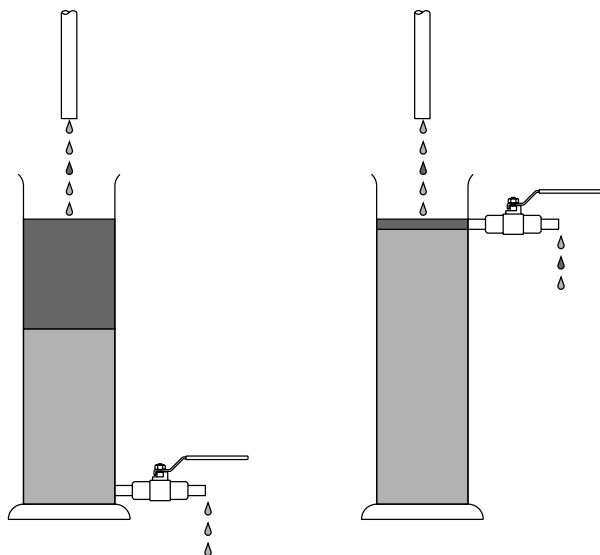


Figure LD-4.

If a beaker collecting oil and water is drained from the bottom at the same rate that oil and water enter, it will eventually fill entirely with oil because oil floats on water.

Figure LD-5.

If a beaker collecting oil and water is drained from the top at the same rate that oil and water enter, it soon will be entirely filled with water because the oil floats on the water.

Air Loss. Often in compressed air systems, the solution to one problem may also cause another problem. For example, a common method of draining unwanted moisture is to crack open a valve; however, this also creates a leak. The immediate problem is solved, but the “solution” has an obvious, and usually underestimated, cost of continual air loss.

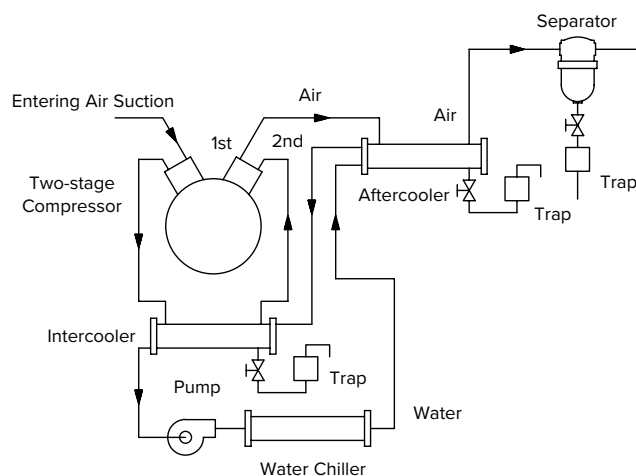
How much air is lost depends on orifice size and line pressure (see Table LD-2). The overall result is a decrease in line pressure, the loss of up to a third of the system’s compressed air, and the cost of compressing it.

Leak control involves:

- Looking for leaks during shut-down with an ultrasonic leak detector
- Determining total leakage by observing how fast pressure drops with the compressor off, both before and after a leak survey
- Fixing leaks at joints, valves and similar points
- Replacing cracked-open valves with drain traps
- Checking the system regularly

Figure LD-6. Drain Trap Locations in a Compressed Air System

The use of drain traps is an effective way to remove water that collects in many places in a compressed air system. Each trap location must be considered individually.



Compressed Air/Gases—Basic Concepts

Drainage Methods

Manual. Liquid may be discharged continuously through cracked-open valves, or periodically by opening manually operated drain valves.

Open drains are a continuous waste of air or gas—and the energy to produce it. A valve manually opened will be left open until air blows freely. Frequently, however, the operator will delay or forget to close the valve, and precious air or gas is lost.

Automatic. Automatic drainage equipment that is adequate for the system is seldom included in the original system. However, subsequent installation of automatic drain traps will significantly reduce energy and maintenance costs.

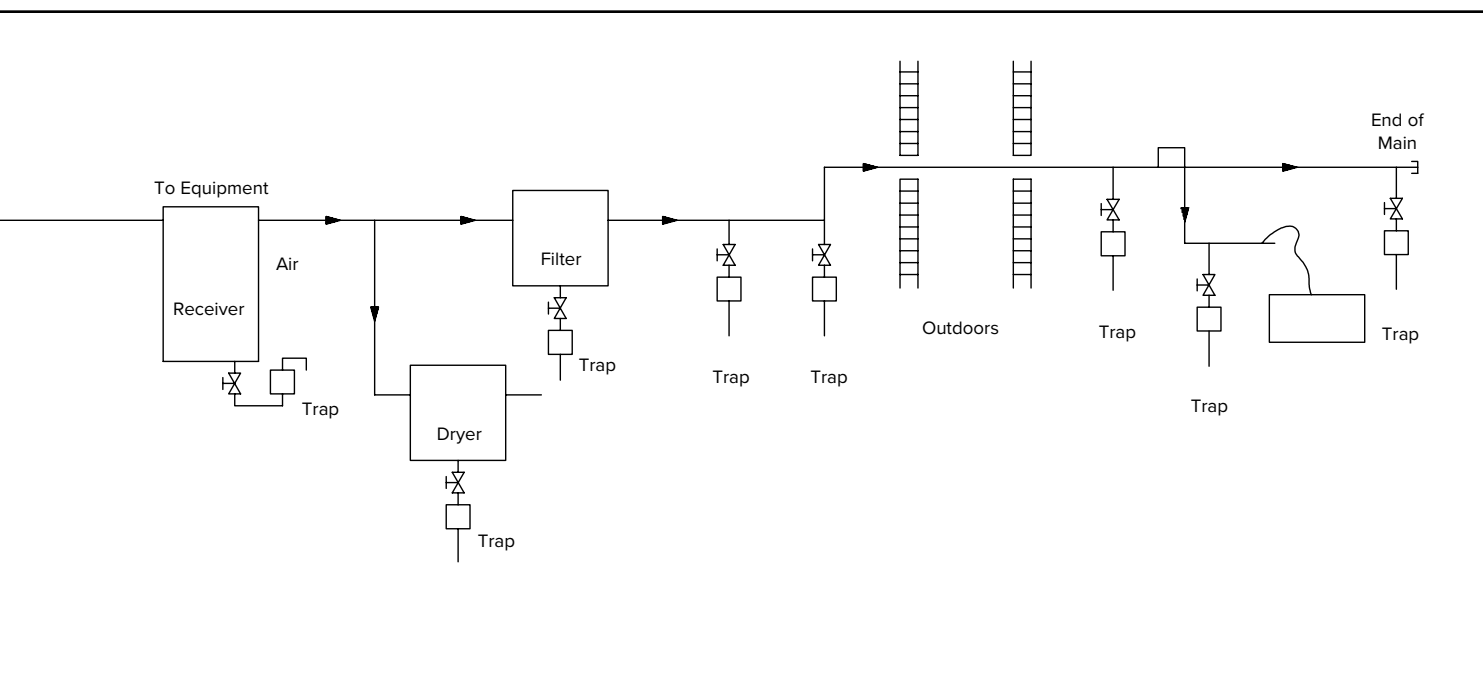
Drain Traps. Water collected in separators and drip legs must be removed continuously without wasting costly air or gas. In instances where drain traps are not part of the system design, manual drain valves are usually opened periodically or left cracked open to drain constantly. In either case, the valves are opened far enough that some air and gas are lost along with the liquid. To eliminate this problem, a drain trap should be installed at appropriate points to remove liquid continuously and automatically without wasting air or gas.

The job of the drain trap is to get liquid and oil out of the compressed air/gas system. In addition, for overall efficiency and economy, the trap must provide:

- Operation that is relatively trouble-free with minimal need for adjustment or maintenance
- Reliable operation even though dirt, grit and oil are present in the line
- Long operating life
- Minimal air loss
- Ease of repair

Table LD-2. Cost of Various Size Air Leaks at 90 psig

Orifice Diameter (in)	Leakage Rate (scfm)	Total Cost Per Month	Cost Total Per Year
3/8	138.00	\$1 207.50	\$14 490
1/4	61.00	533.75	6 405
1/8	15.40	134.75	1 617
7/64	11.80	103.25	1 239
5/64	6.00	52.50	630
1/16	3.84	33.60	403



For Heavy Oil/Water Service

BVSW inverted bucket drain traps are designed for systems with heavy oil or water services.

An inverted bucket is used because the discharge valve is at the top, so oil is discharged first and the trap body is almost completely filled with water at all times.

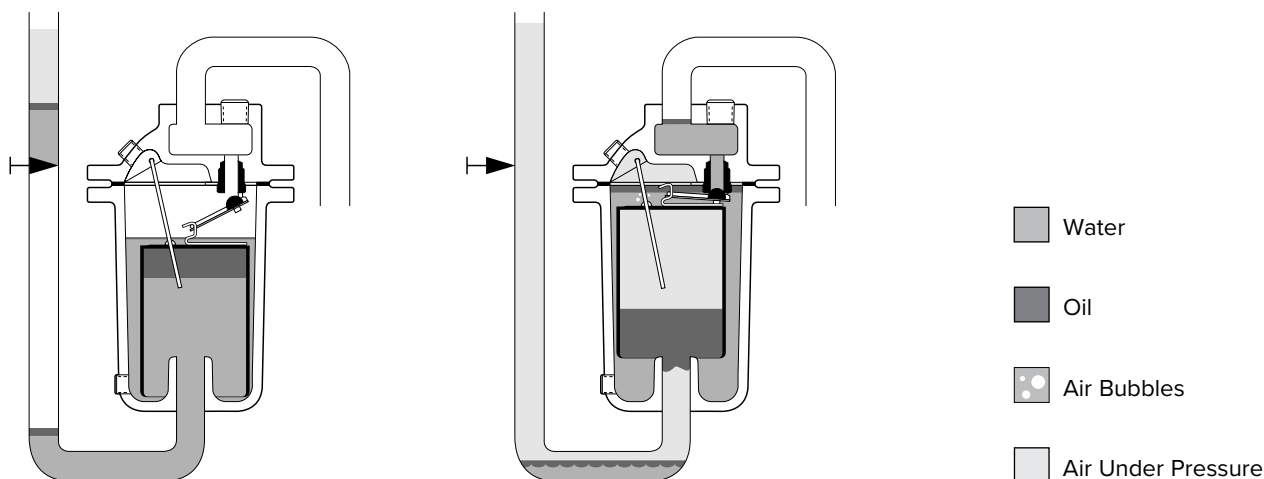
BVSW stands for Bucket Vent Scrubbing Wire. This 1/16" dia. wire swings freely from the trap cap and extends through the bucket vent. Its function is to prevent reduction of vent size by buildup of solids or heavy oil in the vent itself. The up-and-down motion of the bucket relative to the vent scrubbing wire keeps the vent clean and full size.

Operation of Inverted Bucket Drain Traps

1. Since there is seldom sufficient accumulation of water to float the bucket and close the valve, the trap must be primed on initial start-up or after draining for cleaning. Step 1 shows "after operating" primed condition with oil in the top of bucket and a very thin layer of oil on top of water in the trap body.
2. When valve in line to trap is opened, air enters bucket, displacing liquid. When bucket is two-thirds full of air, it becomes buoyant and floats. This closes the discharge valve. As bucket rises, the vent scrubbing wire removes oil and any dirt from bucket vent.

Both liquid and air in trap are at full line pressure, so no more liquid or air can enter trap until some liquid or air escapes through the discharge valve. Static head forces air through bucket vent. The air rises to top of trap and displaces water that enters bucket at bottom to replace air that passes through vent. Just as soon as bucket is less than two-thirds full of air, it loses buoyancy and starts to pull on valve lever as shown in Step 3.

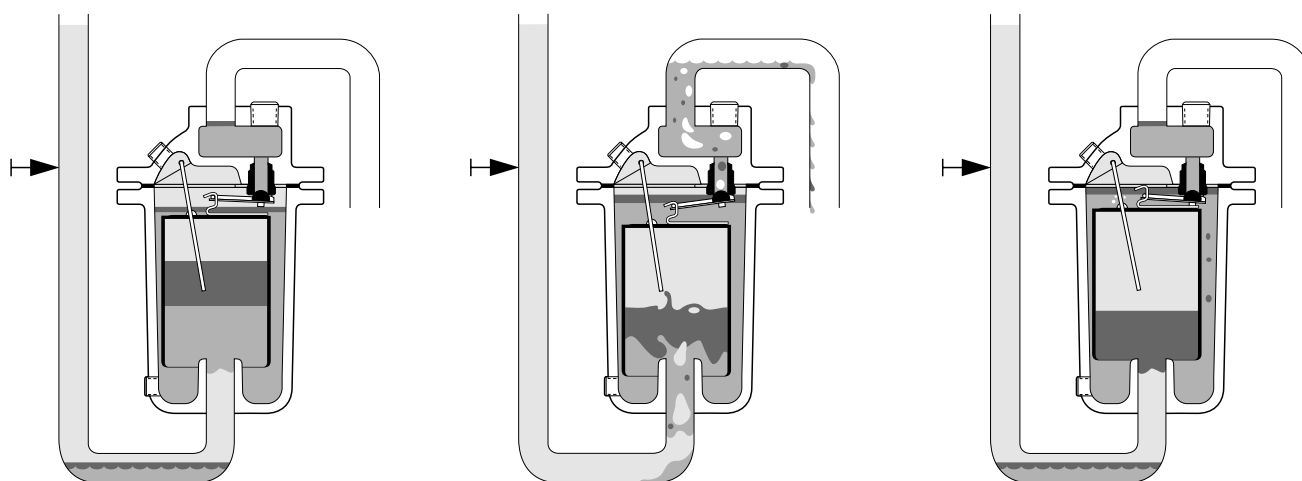
Figure LD-7. Operation of the BVSW Inverted Bucket Drain Trap



1. Trap primed, air off, bucket down, trap valve open.
2. Trap in service, bucket floating. Air passes through bucket vent and collects at top of trap.

Inverted Bucket Drain Traps

3. Note that liquid level at top of trap has dropped and the liquid level in the bucket has risen. The volume of water displaced by air exactly equals the volume of water that entered the bucket. During this valve-closed part of the operating cycle—Steps 2 and 3—water and oil are collecting in the horizontal line ahead of the trap. When the bucket is about two-thirds full of liquid, it exerts enough pull on lever to crack open the discharge valve.
4. Two things happen simultaneously. a) The accumulated air at top of trap is discharged immediately, followed by oil and any water that enters the trap while the valve is cracked. b) Pressure in trap body is lowered slightly, allowing accumulated liquid in horizontal line to enter the trap. Air displaces liquid from the bucket until it floats and closes the discharge valve, restoring the condition shown in Step 2.
5. When full buoyancy is restored, the trap bucket is two-thirds full of air. Oil that has entered while trap was open flows under bottom of bucket and rises to top of water in trap body. The trap normally discharges small quantities of air several times per minute.



3. Water enters bucket to replace air passing through bucket vent. This increases weight of bucket until...
4. ...pull on lever cracks valve. Air at top of trap escapes, followed by oil and water. Liquid in pipe ahead of trap enters bucket followed by air.
5. Air displaces liquid and excess oil from bucket, restoring condition shown in Step 2.

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Closed Float

Hollow, thin-wall metal floats are attached through linkages to valves at the trap bottom, and a seat with an appropriately sized orifice is inserted at the trap outlet. Floats are selected to provide adequate buoyancy to open the valve against the pressure difference. Discharge usually is to atmosphere, so the pressure drop is equal to the system air pressure. The float and linkage are made of stainless steel, and the valve and seat are hardened stainless steel for wear resistance and long life. The body is cast iron, stainless steel, or cast or forged steel depending on gas pressure. Bodies may be made of stainless steel to resist corrosive gas mixtures.

Entering liquid drops to the bottom of the body. As liquid level rises, the ball is floated upward, thereby causing the valve to open sufficiently that outlet flow balances inlet flow. Subsequent change of incoming flow raises or lowers water

level further opening or throttling the valve. Thus discharge is proportionally modulated to drain liquid completely and continuously. However, gas flow may be constant or it may abruptly change depending on system demand characteristics. Liquid formation may be sporadic, or the nature of flow generation may cause surges. At times, flow will be very low, requiring operation to throttle the flow or even tight shut-off. Tightness of closure, gas leakage and trap cost will depend on the design of linkage and valve.

Free Floating Lever

The discharge from the No. 1-LD is continuous. The opening of the valve is just wide enough to remove the liquid as fast as it comes to the trap. Thus, at times, the valve is barely cracked from its seat.

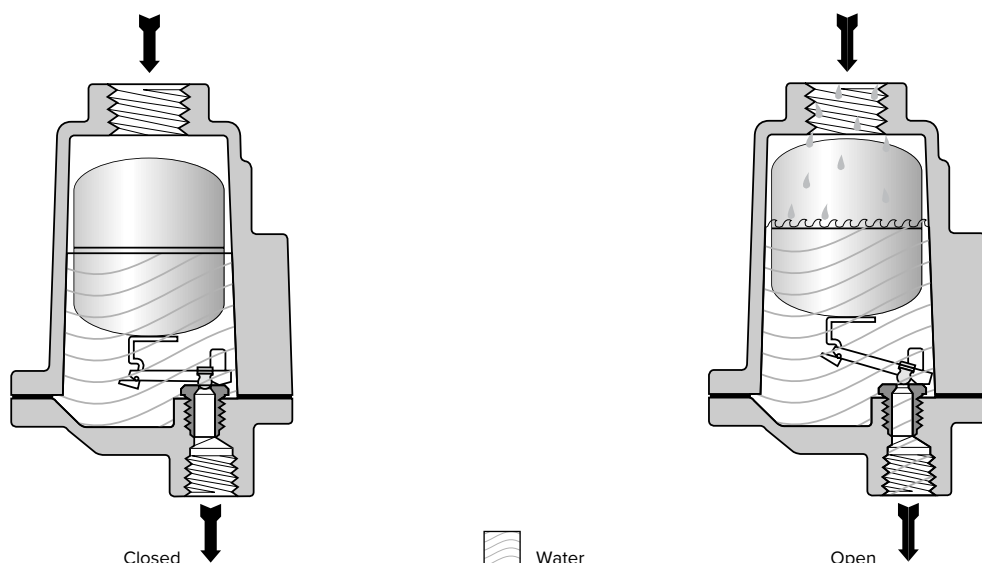


Figure LD-8. Operation of the No. 1-LD Free Floating Lever Drain Trap

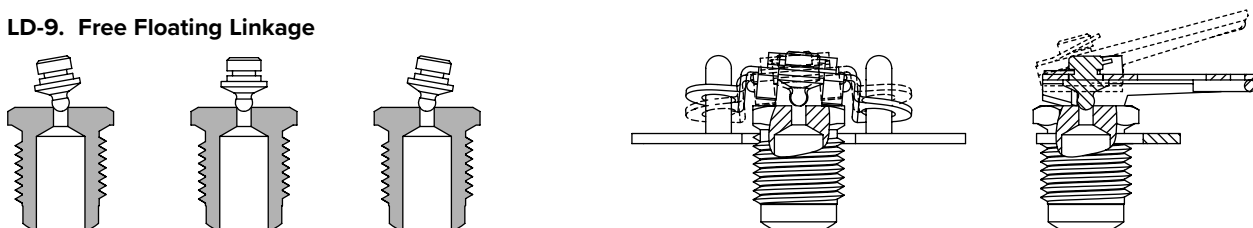
As water begins to fill the body of the trap, the float rises, opening the discharge valve. Motion of the free floating valve lever is guided to provide precise closure.

Free Floating Linkage Valve

A hemispherical ball-shaped valve is attached to linkage which is suspended freely on two guide pins. There is no fixed pivot or rigid guides; therefore, the attachment is loose. There are no critical alignments, and the lever and valve may move in all directions. Consequently, the lever may move the

valve to the seat in any alignment. As the valve approaches the seat, the pressure pushes the round valve into the square edge orifice of the seat, effecting a line seal to attain bubble-tight closure.

Figure LD-9. Free Floating Linkage



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Float Type Drain Traps

Fixed Pivot Conical Valve

A conically shaped valve is attached to a fixed pivot leverage system. The fixed pivot does not allow the valve to move

freely to conform to the seat for tight closure. Thus, it may not seal tightly, and some loss of air or gas may be expected.

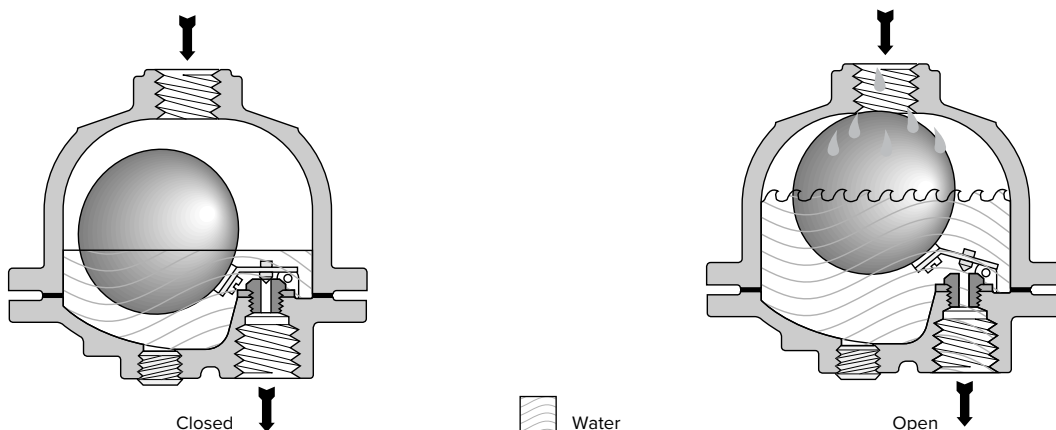


Figure LD-10. Operation of No. 21 Fixed Pivot Drain Trap

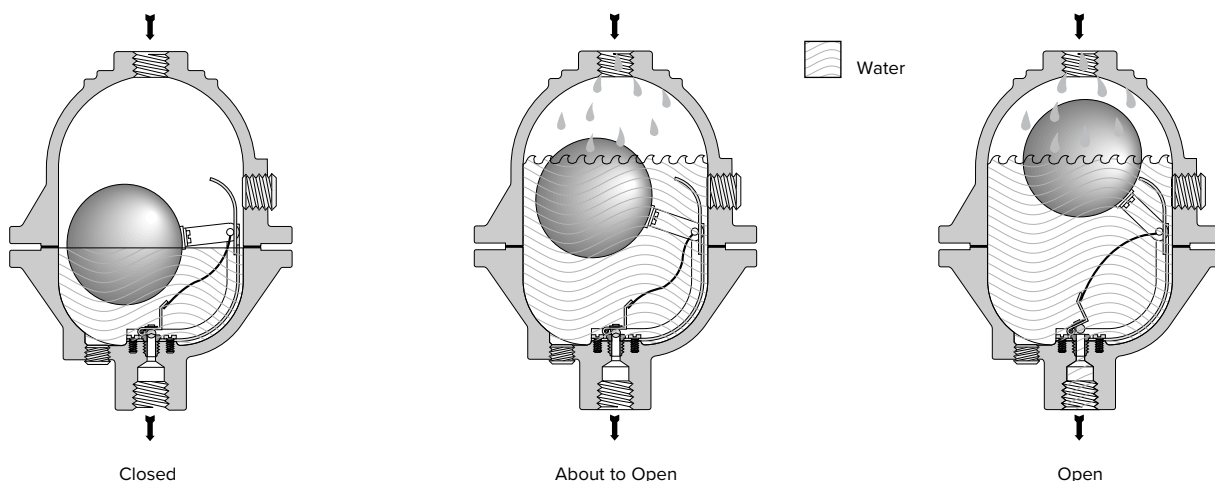
As the water level rises, the ball float cracks the valve to drain liquid at the same rate that it reaches the trap. Changes in the rate of flow to the trap adjust the float level and the degree of opening of the valve.

Snap Action Valve

Because of the sporadic liquid flow, much of the time the valve in a standard float-type drainer is only slightly opened. If there is fine dirt or grit in the liquid, particles may accumulate and clog the partially open valve, or they may lodge between the valve and seat, preventing closure. To overcome this, a special toggle-spring operated valve is used.

A flat spring attached to the leverage system holds the valve closed until liquid level is high enough for the buoyancy to exceed the spring force. Then the valve is snapped open, and the accumulated dirt and grit can be flushed through the wide open valve. When the body is nearly empty, buoyancy is reduced enough to permit the spring to snap the valve closed.

Figure LD-11. Operation of No. 71-A Snap Action Drain Trap



Filling Cycle. Trap valve has just closed. Spring bowed to right. Float rides high in water because no force is exerted on spring. As water enters, float rises, storing energy in spring. This increases submergence of float.

Float now is more than half submerged and spring has assumed a "handlebar mustache" shape. Energy stored in spring is due to increased displacement of water. A very slight rise in water level causes spring to snap to the left...

...Instantly the valve opens wide. This releases energy from spring and float again rides high in water. As water level drops, weight of float bends spring to right, causing snap closing of valve before all the water has been discharged.

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To obtain the full benefits from the traps described in the preceding section, it is necessary that the correct size and pressure of drain trap be selected for each job, and that it be properly installed and maintained.

Rely on Experience. Most drain traps are selected on the basis of experience. This may be:

- Your personal experience
- The experience of your Armstrong Representative or distributor
- The experience of thousands of others in draining identical equipment

Do-It-Yourself Sizing is required at times. Fortunately, drain trap sizing is simple when you know or can figure:

1. Liquid loads in lbs/hr.
2. Pressure differential.
3. Maximum allowable pressure.

1. Liquid Load. Each “How To” section of this handbook contains formulas and useful information on proper sizing procedures and safety factors.

2. Pressure Differential. Maximum differential is the difference between main pressure, or the downstream pressure of a PRV, and return line pressure. See Fig. LD-12. The drain trap must be able to open against this pressure differential.

Operating differential. When the plant is operating at capacity, the pressure at the trap inlet may be lower than main pressure. And the pressure in the return header may go above atmospheric.

If the operating differential is at least 80% of the maximum differential, it is safe to use maximum differential in selecting traps.

IMPORTANT: Be sure to read the discussion on page LD-16, which deals with less common, but important, reductions in pressure differential.

3. Maximum Allowable Pressure. The trap must be able to withstand the maximum allowable pressure of the system, or design pressure. It may not have to operate at this pressure, but it must be able to contain it. As an example, the maximum inlet pressure is 150 psig and the return line pressure is 15 psig. This results in a differential pressure of 135 psig; however, the trap must be able to withstand 150 psig maximum allowable pressure. See Fig. LD-12.

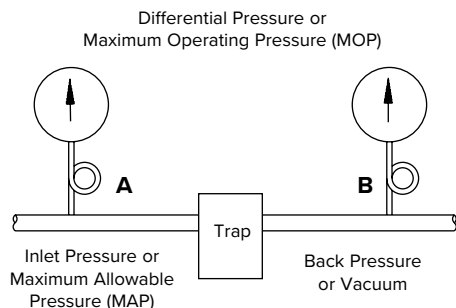


Figure LD-12. “A” minus “B” is Pressure Differential: If “B” is back pressure, subtract it from “A.” If “B” is vacuum, add it to “A.”

Drain Trap Selection

Factors Affecting Pressure Differential

Pressure Differential in Detail

Inlet pressure can be:

1. Air main pressure.
2. Reduced pressure controlled by a pressure reducing valve station.

Discharge can be:

1. Atmospheric.
2. Below atmospheric—under vacuum. Add vacuum to inlet pressure to get pressure differential.
2" Hg vacuum = approximately 1 psig of pressure below atmospheric.
3. Above atmospheric due to:
 - a. Pipe friction
 - b. Elevating liquid

Every 2' lift reduces pressure differential by approximately 1 psig, when the discharge is only liquid.

Special Considerations

Drain traps are available for services other than those found on standard compressed air systems.

High Pressure

Spring-loaded mechanisms allow float type drain traps to operate on pressures above 3 000 psig.

Fluids Other Than Water

Different fluids, such as oils and liquid, can be compensated for with specially weighted floats or lower operating pressure ratings. Fluids with specific gravities down to 0.4 will work with float type drain traps.

Materials of Construction

Service requirements for stainless steel or other corrosion-resistant materials can be met by float and inverted bucket type drain traps.

NACE Sour Gas Service

Special materials and construction are required for hydrogen sulfide service.

High Capacity for Large Flow Rates

Ultra-capacity type drain traps allow float type drain traps to be used on service requiring capacities up to 700 000 lbs/hr.

Dual Gravity

Float type drain traps can be modified to drain a heavier fluid from a lighter fluid.

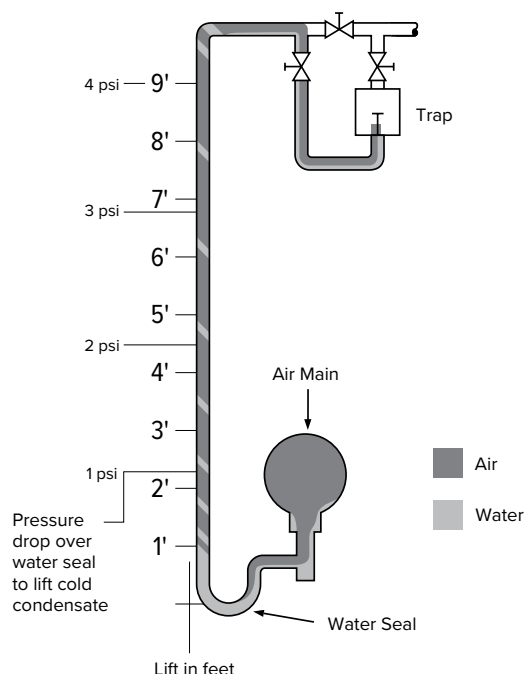


Figure LD-13. Liquid from gravity drain point is lifted to trap by a syphon. Every 2' of lift reduces pressure differential by approximately 1 psig. Note seal at low point and the trap's internal check valve to prevent back flow.

Air distribution systems make up the vital link between compressors and the vast amount of air-utilizing equipment. They represent the method by which air is actually transported to all parts of the plant to perform specific functions.

The three primary components of air distribution systems are air mains, air branch lines, and air distribution manifolds. They each fill certain requirements of the system, and together with separators and traps, contribute to efficient air utilization. Common to all air distribution systems is the need for drip legs at various intervals. These drip legs are provided to:

1. Let liquid escape by gravity from the fast-moving air.
2. Store the liquid until the pressure differential can discharge it through the drain trap.
3. Serve as dirt pockets for the inevitable dirt and grit that will accumulate in the distribution system.

Air mains are one of the most common applications for drain traps. These lines need to be kept free of liquid to keep the supplied equipment operating properly. Inadequately trapped air mains often result in water hammer and slugs of liquid, which can damage control valves and other equipment. There is also a freeze potential wherever water is allowed to accumulate. In areas where air is moving slowly, the accumulation of water can effectively reduce the pipe size, thereby increasing the pressure drop and wasting energy.

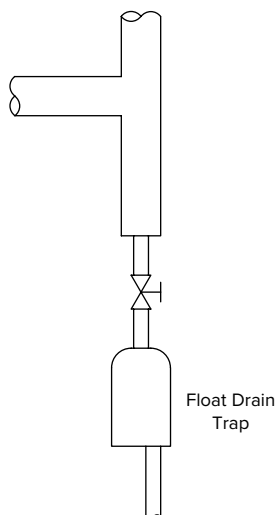


Figure LD-14.
Drain trap installed straight under a low point.

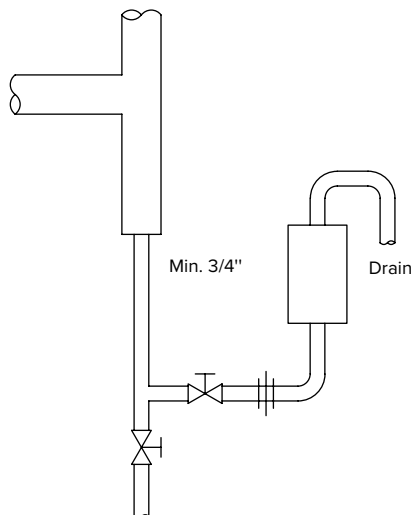


Figure LD-15.
Series 200 or 300 inverted bucket drain traps installed on compressed air line contaminated by oil.

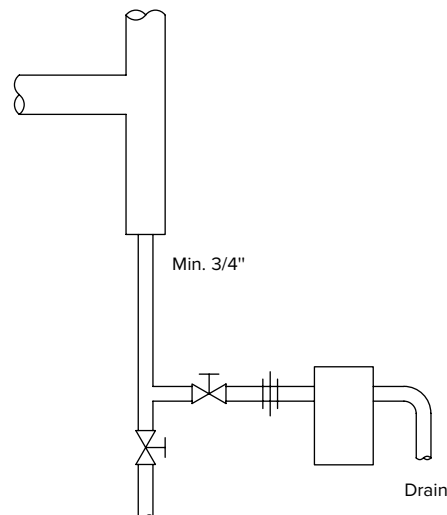


Figure LD-16.
Series 800 or 900 inverted bucket drain traps installed on compressed air line contaminated by oil.

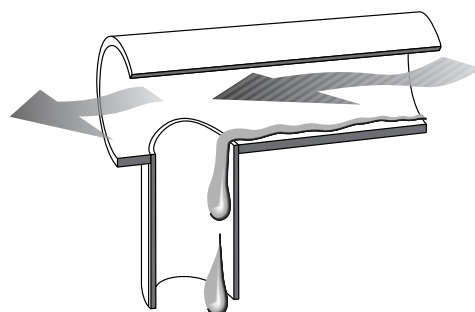


Figure LD-17. Drip leg length should be at least 1-1/2 times the diameter of the main and never less than 10". Drip leg diameter should be the same size as the main, up to 4" pipe size and at least 1/2 of the diameter of the main above that, but never less than 4".

Chart LD-3. Recommendation Chart
(See chart on page LD-6 for "Feature Code" references.)

Equipment Being Drained	1st Choice and Feature Code	Alternate Choice and Feature Code
Air Mains	FF B, C, D, J, M	FP*

*IB is a good alternative where heavy oil carryover is likely.

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How to Drain Air Distribution Systems

Selection of Drain Traps and Safety Factor for Air Mains

Traps should be selected to discharge a volume of liquid normally produced when the system is up and running. Liquid loads can be estimated if actual CFM or air volume flow is not known. If cold temperatures are possible, the dew point at supply pressure must be known. Once this maximum is determined, the safety factor used to size the trap will be only 10% of the total potential liquid load. Ten percent of the total is used because most of the liquid has been removed in the aftercooler and receiver. The drain trap must handle only the small remaining amount of 10% of the total possible load.

If actual airflow rate is not known, it can be estimated using Chart LD-4, titled "Pressure Drop in Compressed Air Pipe." Using an assumed pressure drop of 1/4 (.25) psig per 100 ft, and 100 psig gauge pressure of air through a 4" line, it can be seen that approximately 1 000 cu ft of free air per minute are flowing through the line. Taking this figure to the chart titled "Water Condensed From Compressed Air," Chart LD-6 on page LD-20, it can be seen that if 80°F, 90% RH air is delivered at 100 psig, then 1.2 lbs of water will be condensed per minute at 1 000 CFM. This number will be multiplied by 60 to convert from minutes to hours, which equals 72 lbs/hr. For this air main then, take 10% of this figure, or 7.2 lbs/hr, to be the flow rate to the drainer.

Rule of Thumb for Calculating Compressor Liquid Loads

$$\frac{\text{CFM} \times 20 \text{ gr/cu ft} \times 60 \text{ min/hr}}{7\,000 \text{ gr/\#}} = \text{\#/hr}$$

1. Assuming worst condition:
100°F @ 100% RH
For other conditions, see page LD-7
2. Using air main safety factor of: Load x 10%

Installation of Drain Traps on Air Mains

Drip Legs. All air mains should utilize drip legs and traps at all low spots or natural drainage points, such as ahead of risers, end of mains, ahead of expansion joints or bends, and ahead of valves and regulators (see installation Fig. LD-17).

Where there are no natural drainage points, drip legs and drain traps should still be provided. These should normally be installed at intervals of about 500 ft.

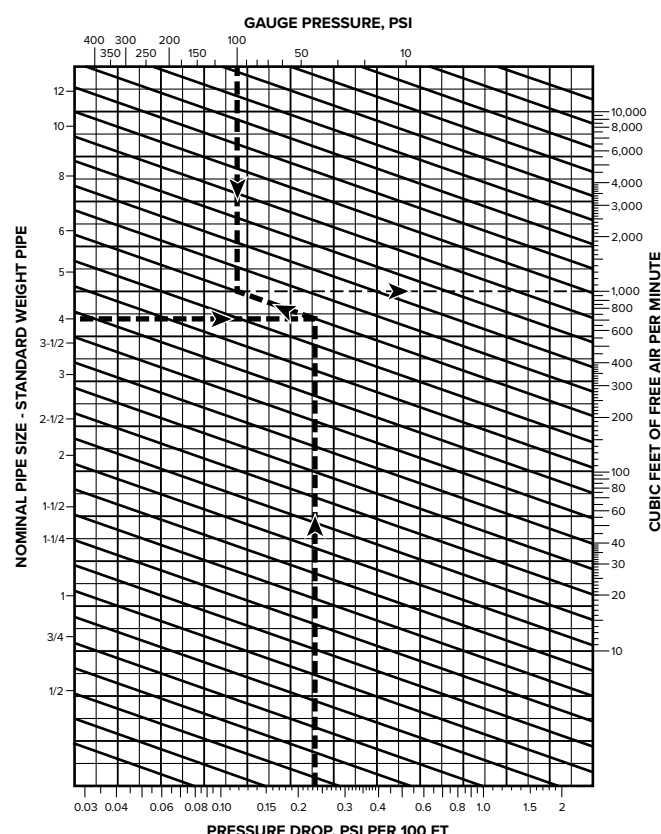


Chart LD-4. Pressure Drop in Compressed Air Pipe

Chart gives pressure drop in compressed air piping in pounds per square inch per 100 ft of pipe. Initial pressure, flow and size of pipe must be known or assumed.

Branch Lines

Branch lines are takeoffs of the air main supplying specific areas of air-utilizing equipment. Branch lines must always be taken from the top of the air main. The entire system must be designed and hooked up to prevent accumulation of liquid at any point. If a specific process area requires it, an air dryer will be installed on the branch line.

Trap Selection and Safety Factor for Branches

The formula for computing liquid load in branch lines is the same as that used for air mains. Branch lines also have a recommended safety factor of 10% of total air load. Drip legs must be installed ahead of risers and at the end of branch lines, especially when branch line runouts exceed 50 ft. There are usually several branches off the air main, and in many cases they experience a high liquid load when they run against cold outside walls. This cooling causes more moisture to condense in the branch line than would be seen in the air main.

Distribution Manifolds

A distribution manifold is a terminal for a branch line from which several air users are taken off. They are particularly common in manufacturing facilities for pneumatic tool hookups or takeoffs to cylinder actuators. Like branch lines, it is common for distribution manifolds to be installed against cool walls where low temperatures cause condensation and the accumulation of liquid.

Distribution manifolds are often equipped with filters and regulators. Regulators may also be found at the termination before the air-using device.

Since the air distribution manifold is usually one pipe size larger than the branch line, it is common for air velocity to drop when coming from the branch line. With this decrease in velocity, often combined with lower ambient temperatures, it is common for a liquid to accumulate in the distribution manifold. For this reason, the use of filter-drainer combinations or separate drain traps is recommended. Trapping the liquid in the distribution manifold is important to protect the regulators on air-using equipment and orifices in air-using instruments.

This is a location where manual valves are commonly misused due to their accessibility. To drain the liquid and keep it from fouling an instrument or pneumatic tool, manual valves will often be cracked to atmosphere. When they are left this way, the result is a large air loss due to the unrestricted free blow of air to atmosphere.

Trap Selection and Safety Factor for Distribution Manifolds

Normally the smallest drain trap is practical for distribution manifolds up to manifold diameters of 2". Above 2", the distribution manifold should be considered a branch, and then the sizing procedure from the Air Main section would apply.

Chart LD-5. Recommendation Chart
(See chart on page LD-6 for "Feature Code" references.)

Equipment Being Drained	1st Choice and Feature Code	Alternate Choice
Branch Lines	FF B, C, D, J, M	FP*
Distribution Manifolds	FF B, C, D, I, M	FP

*IB is a good alternative where heavy oil carryover is likely.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

How to Drain Air Distribution Systems

Installation

The ABCs of trap installation must be followed: “A” for accessible, “B” for below the point being drained, and “C” for close to the point being drained. If the discharge point for this drain trap is some distance away from the drain point, the discharge line from the trap should be run out—not the inlet to the trap.

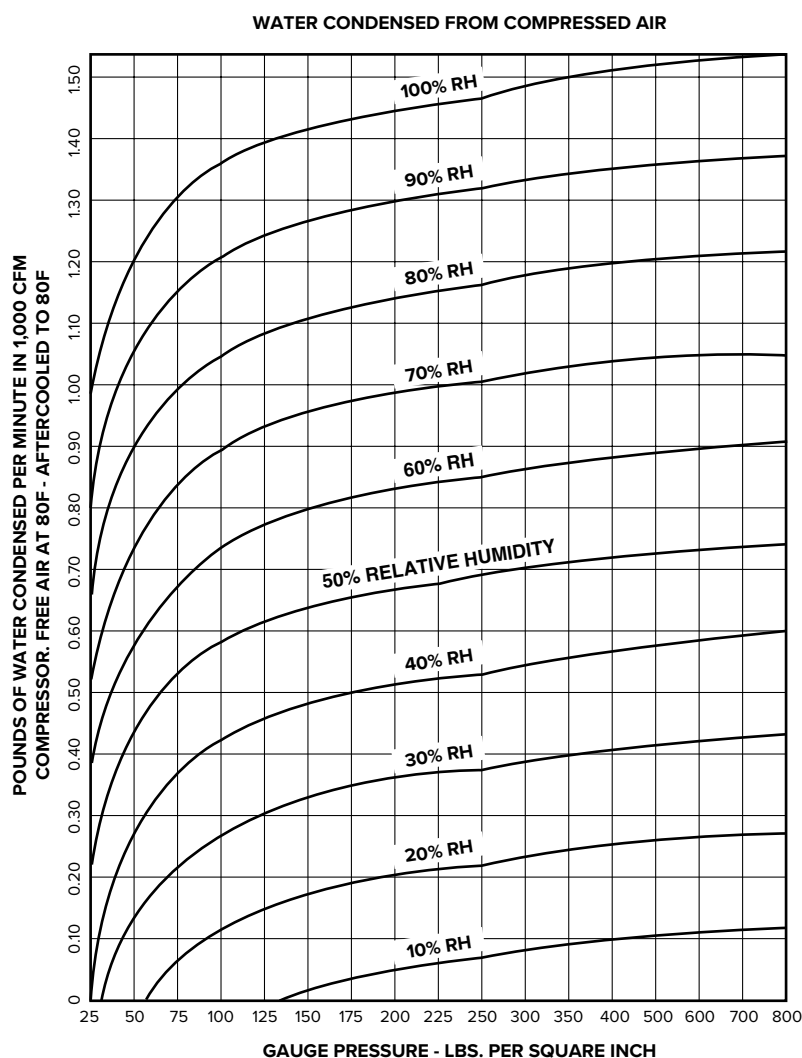
When installing traps on the drain connection of filters, particular care should be taken to the connection size. Normally outlet connections on filters are 1/4" in size or less. This connection size is normally not large enough to allow anything but slugs of liquid to flow into the trap housing. If a float trap is utilized, it should be either back vented or the connection size must be increased to 3/4" minimum. For additional installation recommendations, see pages LD-51 and LD-52.

Table LD-3. Correction Factors

For lbs water condensed at temperatures other than 80°F, find wt condensed at 80°F and multiply by factors shown.

°F	Factor	°F	Factor	°F	Factor	°F	Factor
10	.070	50	.373	100	1.81	140	5.15
20	.112	60	.525	110	2.39	150	6.52
30	.176	70	.729	120	3.12	160	8.19
40	.259	90	1.35	130	4.02	170	10.2

Chart LD-6. Water Condensed From Compressed Air



NOTE: Amount of water condensed is in direct ratio to compressor rating. For example, for 500 CFM compressor, multiply determined amount of condensate by 0.50; for 200 CFM compressor, multiply amount of condensate by 0.20.



How to Drain Intercoolers, Aftercoolers, and Aftercooler Separator Combinations

Aftercooler

An aftercooler serves as the primary means of moisture removal on industrial air systems. It increases the efficiency of air distribution by reducing pressure drop created when air flows through the system. It does this by using cooling water to reduce the specific volume of the air which, in turn, allows the air to flow through the system with less pressure drop. Aftercoolers are found on most industrial compressors over 10 hp in size. In addition to removing the heat of compression, aftercoolers also remove approximately two-thirds of the liquid found in the air, and help in the removal and knock-down of oil carryover from the compressor.

Intercooler

Compressor intercoolers are designed to increase the efficiency of compression by reducing the temperature and specific volume of air between stages of compression. This allows the compressor to do more work at a lower temperature than would normally occur. Because some condensing will occur in the intercooler, a drain trap is required to protect compressor parts.

If liquid were to carry over from the intercooler, it could also carry dirt or scale into the compressor and/or also cause corrosion within the compressor, both of which are undesirable for efficient compressor operation. If slugs of liquid were to pass from the intercooler into the compressor, it would make the compressor operation erratic. Efficient trapping is required at this point to deliver dry air to the next stage of the compressor.

An intercooler is typically a shell and tube heat exchanger. Liquid condensate flow out of the heat exchanger is usually irregular, causing slugs to accumulate and pass into the drain trap. Because of this, a drip leg is required on the intercooler,

and full size outlet piping from the intercooler must be used into a dirt pocket. The drip leg allows the slug of condensate to be handled by the drain trap and handles some small backup while the drain trap is discharging the liquid.

The intercooler may also experience oil carryover if the compressor is not of the oil-less or sealed type. As air enters the intercooler, it carries a mist or tiny droplets of oil along with it. Because the air is at a relatively high temperature, this oil is fairly thin. Then, as the intercooler cools the air and oil, the oil may thicken. The drain trap must be able to discharge this oil before it thickens and negatively affects the drain trap and intercooler operation. Trap selection is very important in this type of application where a water and oil mix must be handled by the trap and the oil must be discharged first.

Since the aftercooler removes approximately two-thirds of the total moisture load, traps here will normally be much larger than those found on the rest of the system.

Trap Selection and Safety Factor

Intercooler

Select the proper trap for:

1. Entering water temperature into the intercooler.
2. Airflow rate through the intercooler.
3. Intermediate pressure at which the intercooler is operated.

Use Chart LD-6 on page LD-20, "Water Condensed From Compressed Air," to determine the pounds of water condensed per minute in 1 000 CFM. Then multiply by 60 to convert minutes to hours and use a safety factor of 2:1.

Chart LD-7. Recommendation Chart
(See chart on page LD-6 for "Feature Code" references.)

Equipment Being Drained	Air		Gas	
	1st Choice and Feature Code	Alternate Choice	1st Choice and Feature Code	Alternate Choice
Aftercooler	IB F	FF	*FF	FP
Intercooler	, G, J, K, M		B, E, J	

*Since IBs vent gas to operate, an FF is suggested because gas venting may not be desirable.

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How to Drain Intercoolers, Aftercoolers, and Aftercooler Separator Combinations



When selecting the type of trap, consider the failure mode and the ability of the trap to respond to slugs of liquid. In most cases, an “open” failure mode will be desirable as it is vital to protect the compressor from slugs of liquid. A quick response to slugs is important so there is no delay between the time the liquid accumulates and the trap discharges the liquid.

Aftercooler

When the aftercooler condensing rate is not known, there are two typical methods for calculating condensate load. The first method is to calculate total airflow through the system. Then using Chart LD-6 on page LD-20, titled “Water Condensed From Compressed Air,” determine pounds of water condensed per minute in 1 000 CFM. Multiply this by 60 to convert minutes to hours for required trap capacity in pounds per hour (the entering maximum incoming summertime temperature and relative humidity must be known to use this chart). This load is then multiplied by 2 to determine required trap capacity.

The second method of calculating trap capacity is to look at maximum allowable flow rate through the aftercooler. Use the “Water Condensed From Compressed Air” chart on page LD-20 in the same manner as described in Method 1. Although this method will normally yield a larger trap size, it allows for the addition of another compressor or the interconnection of several compressors to the system in the event of unplanned by-passes.

In the second method, it’s important to estimate the average

water temperature within the aftercooler as closely as possible. Not all air actually comes in contact with the water tubes; therefore, the air is not uniformly cooled to the water temperature. If actual leaving air temperature is known, this is by far the most accurate figure to use. A properly sized aftercooler will normally cool compressed air down to within 15°F of entering air temperature.

Installation

When installing drain traps on aftercoolers or aftercooler separator combinations, the “ABCs” of trap installation should be followed:

- A**ccessible for maintenance and repair.
- B**elow the point being drained.
- C**lose to the drip point as possible.

Be sure to follow manufacturer’s instructions on trap installation. Most aftercoolers are equipped with a separate separator. However, if a separator is not furnished, the aftercooler must be trapped individually. In the case of the aftercooler/separator combination, only the separator normally requires a trap. See Fig. LD-18 or LD-19. But again, it is important to follow manufacturer’s instructions. For additional installation recommendations, see pages LD-51 and LD-52.

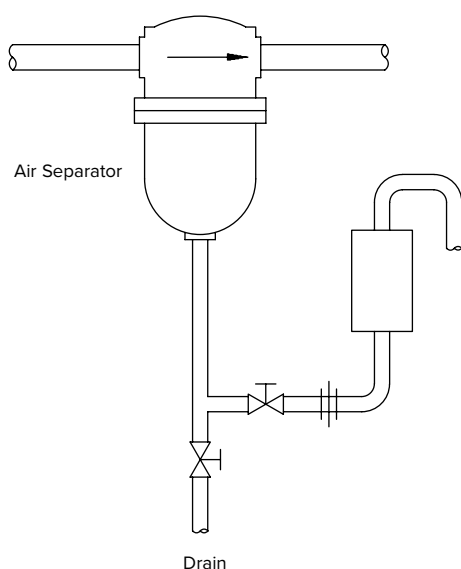


Figure LD-18. Installation of a 200 Series inverted bucket drain trap on compressed air contaminated by oil.

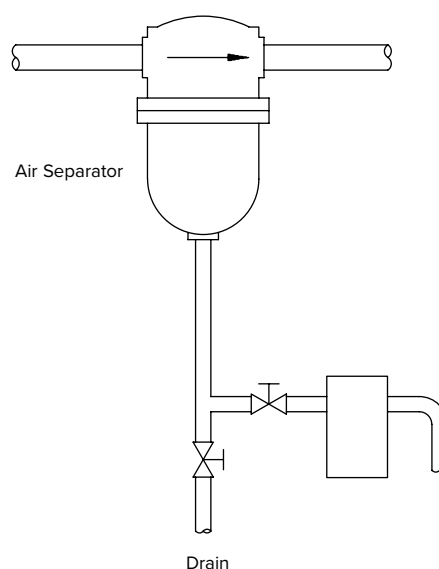


Figure LD-19. 800 Series inverted bucket drain trap installed on compressed air contaminated by oil.

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How to Drain Separators, Separator Filter Combinations

Separators serve an important function within the compressed air system. Separators may also be known as knockout pots, knockout drums or demisters. Their function is to remove liquid that may be moving at a high speed from the flowing air, and they normally perform this function in a two-step process.

1. Separators increase the flow area and volume of the gas, thereby reducing its velocity. Air within the system may flow at velocities exceeding 100 mph. At this velocity any liquid will be entrained as droplets and will not be flowing along the bottom of the pipe. To remove these liquid droplets, it is necessary to reduce the velocity of the gas; otherwise, the droplets accumulate and again become entrained with the flowing gas.
2. The second step is to change direction and impinge the liquid. As the velocity of the gas is reduced, the velocity of the fast-moving droplets can be reduced even further by causing the air to take either 90-degree turns or to centrifugally flow within a chamber. Both of these methods serve to “sling” the droplets up against baffles, plates or the wall of the separator.

Because the droplets have a relatively high mass and are incompressible, their velocity will drop dramatically. At this point, gravity will take over, causing the drops to accumulate and flow into the bottom of the separator. Liquid will often fall in sheets down the wall of the separator and collect at the outlet piping in slugs. The immediate drainage of the slugs is important since the separator is normally a final opportunity to protect an air-using device downstream.

If liquid is allowed to accumulate for any amount of time, it may undermine the entire purpose and function of the separator. Therefore, if the separator does not do its job efficiently, it can actually become a reservoir that accumulates condensate and forms slugs to be transmitted down the air line and into the device being protected. In this case, the use of a separator may be worse than no protection at all.

Locations

Separators are normally located on the leaving side of aftercoolers and before the compressed air receiver. They are often integral with filters located before sensitive air-using equipment or as part of the filter on a distribution manifold. In this case there may be a combination filter, oiler, regulator and separator drainage point for liquids to accumulate.

Trap Selection and Safety Factor

If the separator is part of an aftercooler combination installed between the compressor and the receiver, you should refer to the section on Aftercoolers and Aftercooler Separators for trap selection.

Trap selection is fairly critical, especially on equipment with **larger than 1"** air lines feeding it, since slug formation can wash scale into the air-using equipment and become a serious dirt problem. Therefore, on larger than 1" separators, the flow should be calculated by totaling the air consumption of the devices downstream and using Chart LD-6, “Water Condensed From Compressed Air,” on page LD-20. Use the full water load expected and the safety factor of 3:1 to figure trap capacity.

Chart LD-8. Recommendation Chart (See chart on page LD-6 for “Feature Code” references.)		
Equipment Being Drained	1st Choice and Feature Code	Alternate Choice
Separator Line Size > 1"	FF* J, B, C, E	IB
Separator Inlet Pipe < 1"		FP*

*IB is a good alternative when heavy oil carryover is likely.

How to Drain Separators, Separator Filter Combinations



To determine proper trap capacity for separators with a pipe size of **less than 1"**, the flow can be estimated by using Chart LD-6, "Water Condensed From Compressed Air," on page LD-20, and then calculating 20% of full load.

The safety factor for both selection procedures is 3:1 since separators must respond to surges of liquid from the inlet. In this case, the trap must handle far more liquid than would be experienced under normal operation.

Installation

When installing ball float type traps on separators 1" and above, it's important to back vent the trap (refer to the section on how to hook up ball floats for the purpose and function of back vent lines, page LD-51). All other types of drainers should be coupled as closely as possible to the drain leg. The drain leg should be the same size as the drain connection on the separator and extend 6" below the separator with another 6" allowed for a dirt pocket. The trap is then tee'd off this line (see Figs. LD-20 and LD-21). This piping is crucial because, as noted above, if the separator does not receive full drainage, it can be worse than no separator at all. For this reason, the "ABCs" are critical:

- A**ccessible for inspection and maintenance.
- B**elow the equipment being drained.
- C**lose to the drain point.

The line size leading from the drip leg to the inlet of the unit should be kept the same size as the trap inlet for good drainage into the trap. Again, when slugs are being handled it's important that the trap begin draining immediately. Back vents on float type traps should be a minimum of 1/2" in pipe size with 3/4" preferred. Any valves used in this back-vent piping should be full ported to allow free gas flow out of and liquid flow into the drain trap. For additional installation recommendations, see pages LD-50 to LD-52.

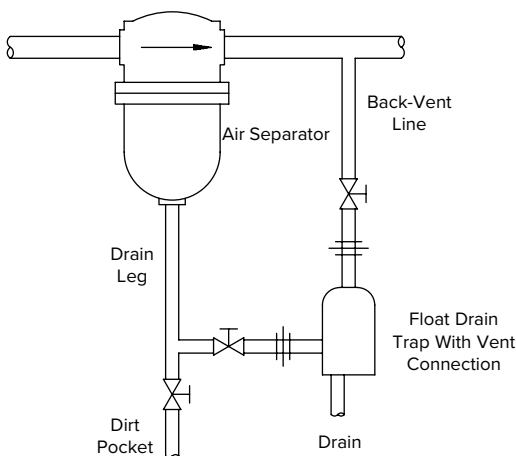


Figure LD-20. Installation of a drain trap with equalizing line downstream of the separator in order to assure a quick and regular flow to the drainer. Note side inlet connection from separator.

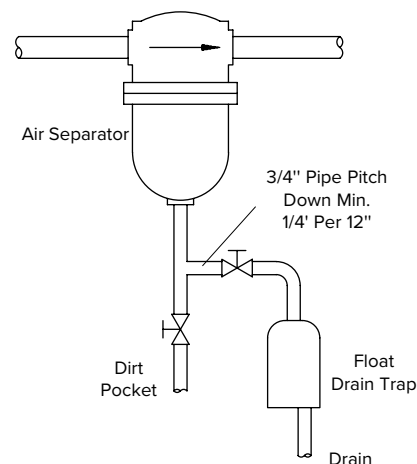


Figure LD-21. Installation of a drain trap on side of separator.

Receivers perform the vital function of storing air for the system. The receiver dampens pressure fluctuations in the system and provides a very short storage time in the event of compressor failure. It also functions as a liquid knockout drum to prevent entrained liquid (which may carry over) from entering the compressed air dryer or the air mains. The receiver should be sized to provide enough storage time for an orderly shutdown, particularly in the case of instrumentation air systems. Receiver volume is what provides the amount of air required for storage periods.

The receiver should be located close to the compressor. Fallout of liquid is normal due to low velocity within the receiver. Velocity is at the lowest point it will reach in any other part of the operating system. The air has a high dwell time within the receiver and is more likely to cool to ambient. This cooling of the air is what causes moisture to condense.

The receiver is equipped with a drain port at the bottom to allow liquids to flow to drain traps. In many cases, because receivers are so large and located adjacent to the compressor, they are installed close to the floor. When this happens, the drain point is relatively inaccessible, making trap piping difficult and gravity flow into the trap often impossible. To avoid this, the receiver should be located on a small concrete pad, which will facilitate efficient drain trap installation and operation.

For several reasons, it's good to keep the receiver drained. When receiver volume is lost, the dampening of the compressed air pressure is reduced and the storage time between compressor failure and system shutdown is greatly reduced. Corrosion within the receiver can also take place when liquid is allowed to accumulate.

Manual valves are commonly used to drain receivers since they are typically installed close to the floor. The resulting loss of receiver volume is seldom noticed in the day-to-day operation of the system. However, with any manual system, the valve can be forgotten and not opened. Then, when the weather changes from a relatively dry, low moisture load to a warm, high moisture load, the receiver will lose volume and the dampening effect and accumulator effect are decreased. The compressor can short cycle under these conditions, increasing the wear and tear on the compressor. In addition, the only reminder to open the manual valve is when carryover occurs. In this case, an air dryer can be damaged, liquid can be introduced into the air mains and surge through the system, causing scale to be washed into the system, water hammer and/or freeze damage.

Trap Selection and Safety Factor

To select the proper trap for the receiver, it is necessary to calculate total system load using Chart LD-6, "Water Condensed From Compressed Air," on page LD-20. Once this total potential load is known, it will be multiplied by the following factors: With an aftercooler, multiply the load by 50%, with an aftercooler separator combination, multiply the total load by 40%, and if no aftercooler is present, multiply the total load by 70%. Once this load is known, a safety factor of 2:1 is applied.

Table LD-4. Total System Load Multipliers

Calculate Total System Load with	Aftercooler	Aftercooler Separator	None
Multiply by	50%	40%	70%

Chart LD-9. Recommendation Chart

(See chart on page LD-6 for "Feature Code" references.)

Equipment Being Drained	1st Choice and Feature Code	Alternate Choice
Receivers	FS* C, E, I, J, K	IB D

*FF for over 120 lbs/hr load.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

How to Drain Receivers

Installation

When a float type drain trap is used with a receiver, the level will run at about the inlet connection on the trap. Therefore, it is important to locate the trap as close to the floor as feasible and with no dips in the piping. See Figs. LD-22 thru LD-25. If there is a piping dip with a float type unit and the vent connection is not back vented, the unit will fail to operate. In the case of a back-vented unit, the dip in the piping will be flooded at all times. An inverted bucket trap can be installed above floor level since it will operate above the drain point. An

internal check valve, tube and coupling should be installed to prevent the liquid seal from flowing backward on system shutdown. A snap action type float unit should be used when any amount of grit is expected in the system. In this case, the spring life can be extended by moving the drain trap slightly upward to allow liquid to accumulate both within the receiver and within the trap body between trap cycles. For additional installation recommendations, see pages LD-50 to LD-52.

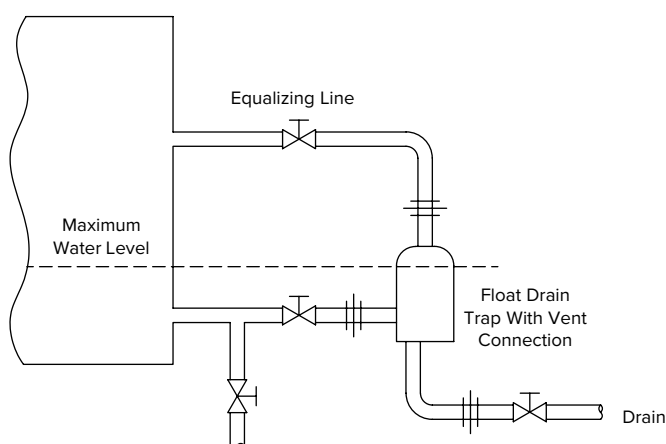


Figure LD-22.

Drain trap installed at side of a receiver, close to floor. Water will rise to broken line before drain trap opens.

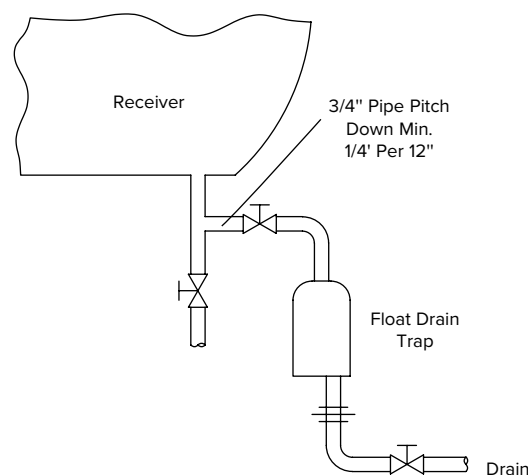


Figure LD-23.

Install the drain trap on side to get better access or compensate for lack of space under the receiver (particularly for drain trap used under compressors).

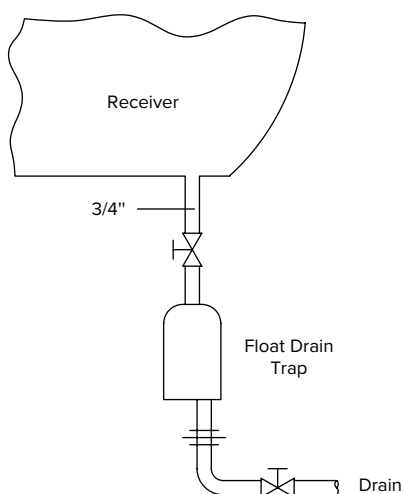


Figure LD-24.

Installation **not recommended** because of the dirt problem that can occur with a drain trap installed straight under the receiver.

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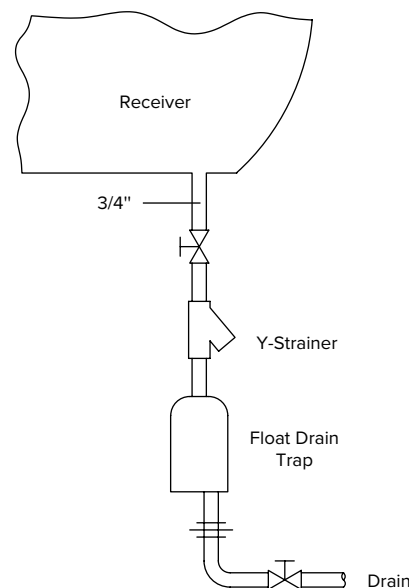


Figure LD-25.

Same installation but with a strainer protecting the drain trap.

The function of dryers is to eliminate liquid in applications where freezing or any moisture accumulation can cause serious problems with the air-consuming equipment. Dryers should always be installed on instrument quality air systems.

Two basic dryer types are dessicant and refrigerated. In the dessicant type, the dessicant chemical absorbs the liquid by chemically bonding with the water molecules. Dessicant dryers can achieve very low dew points and are often installed with a pre-dryer of the refrigerant type. Refrigerant dryers work the same as aftercoolers by circulating cold fluid, causing the moisture to condense. However, their ability to reach low dew points is limited by the temperature at which frost will form on the heat exchanger tubing (greatly reducing heat transfer).

This leads to a discussion of air dew point. Dew point is the temperature at which moisture will condense out from the air due to its relative humidity increasing above 100%; see Chart LD-11. When this happens, the moisture condenses out and can be drained to a drain trap. Dew point is also important when considering air that has left the dryer, because if the air is ever exposed to temperatures below its dew point, moisture will form. Therefore, when applying air dryers, it is important to consider two features of compressed air usage that will impact dryer selection.

1. When air is compressed, the dew point is increased. Also, the dew point under pressurized conditions must be known. For example, even though a -40°F dew point is achieved at atmospheric conditions, this becomes a dew point of about 10°F once the air has been compressed to 100 psig. In outdoor systems, when the temperature drops below 10°F, condensing and freezing of that moisture will result.
2. When compressed air is expanded through instruments or air tools, its volume increases, pressure decreases and a temperature drop is usually experienced. If the temperature drops below the dew point of the air, undesirable moisture forms in the equipment. The air would never be subjected to that temperature under any conditions other than when expanding.

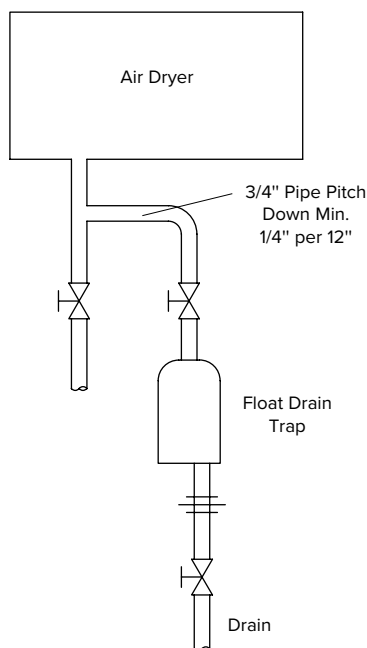


Figure LD-26.
Drain trap installation with dirt leg for purging the dirt.

Chart LD-10. Recommendation Chart
(See chart on page LD-6 for "Feature Code" references.)

Equipment Being Drained	1st Choice and Feature Code	Alternate Choice
Dryers	FF B, C, J, N	IB FP

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How to Drain Dryers

Drain traps are usually required on refrigerated type dryers only. Here the refrigerant chills air and creates moisture that the drain trap can discharge. In the case of the dessicant type air dryer, the chemical grabs the moisture and bonds chemically with the water molecules, and no liquid accumulates. These bonded water molecules are then usually driven off in a regeneration cycle the dryer must periodically undergo.

Trap Selection and Safety Factor

In most cases, the dryer manufacturer will rate the dryer for a given moisture removal rate. The safety factor should still be applied to this load, however. If the manufacturer's ratings are not known, then it's necessary to calculate the moisture content of the air at aftercooler conditions and the moisture content at ambient conditions. Using the lower moisture content between these two, compare that figure to the moisture content at the dew point of the air leaving the dryer. The difference in these moisture contents is then multiplied by the airflow through the dryer to determine the moisture load. The safety factor applied to the load is 2:1 since liquid should be drained immediately from the dryer and the liquid tends to flow into the drain trap in slugs.

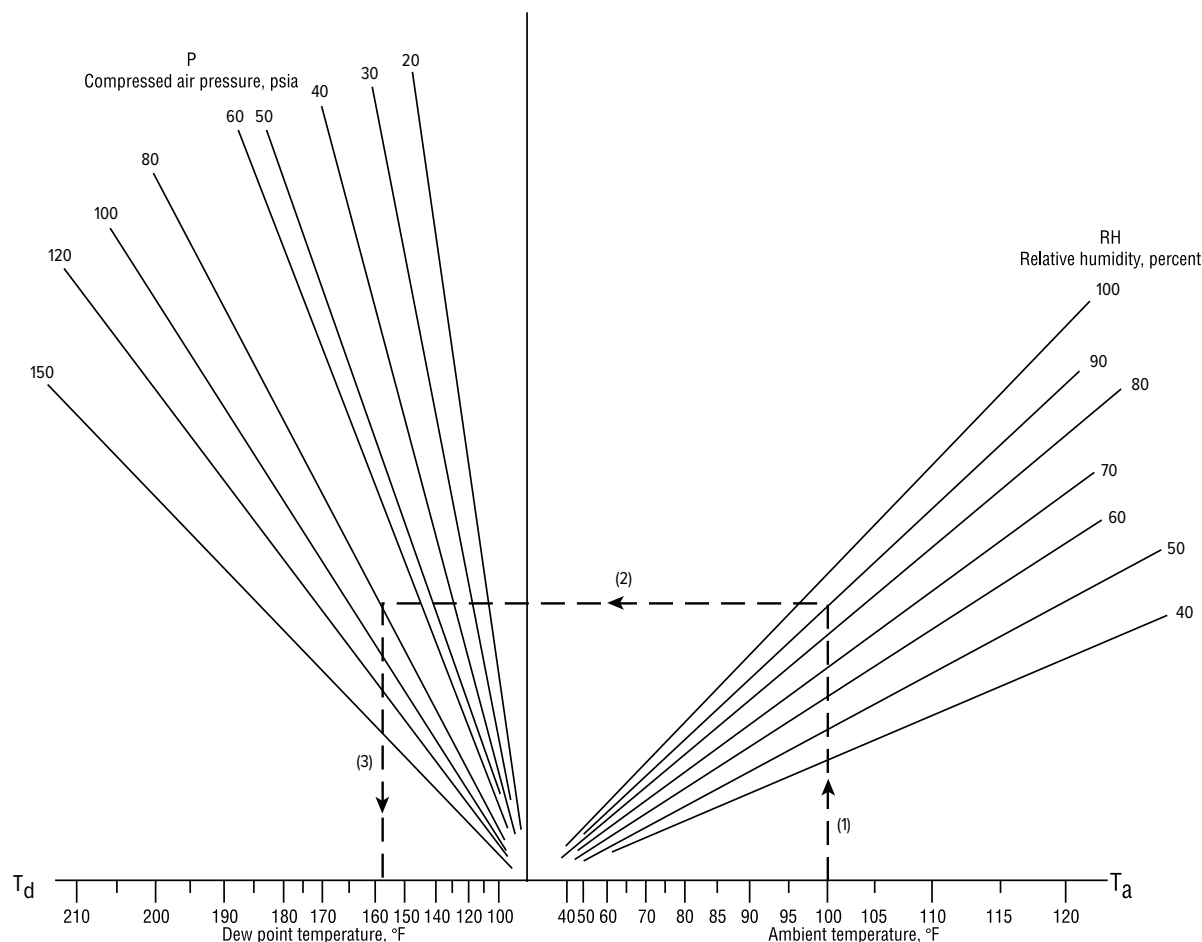
Installation

The dryer should come with a drain port of a given pipe size sufficient to handle the liquid coming out of the dryer. In this pipe size, a drain leg should be piped up 6" below the dryer with another 6" below that as a dirt pocket. Teeing off this line and into the trap with the same inlet size as the trap will allow for gravity drainage into the trap. Again, the ABCs of trap installation should be followed:

- A**ccessible.
- B**elow the point being drained.
- C**lose to the drain leg as possible.

If the trap is too close to the floor to allow the use of a ball float trap, an inverted bucket trap should be considered. For additional installation recommendations, see pages LD-50 to LD-52.

Chart LD-11. Estimated Dew Point of Compressed Air



Nomograph estimates dew point of compressed air.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



How to Select and Size Armstrong Drain Traps

For Draining Liquids From Gases Under Pressure

Armstrong liquid drain traps are offered in a wide variety of sizes and types to meet the most specific requirements. The most widely used models and sizes utilize bodies, caps and some operating parts that are mass produced for Armstrong steam traps. The proven capabilities of these components, along with volume production economies, enable us to offer you exceptionally high quality at attractive prices. You can choose the smallest and least costly model that will meet your requirements with confidence.

Selection Procedure for Draining Liquid From Gas

1. Multiply the actual peak liquid load (lbs/hr) by a safety factor of at least 1-1/2 or 2. See paragraph headed "Safety Factors."
2. From Orifice Capacity Chart LD-12, find the orifice size that will deliver the required cold water capacity at the maximum operating pressure. If a light liquid is to be drained, convert light liquid capacity in lbs per hour to water capacity using factors in Table LD-5. Then find orifice size from Chart LD-12.
3. From the Orifice Size Operating Pressure tables on the product model pages, find the drain trap(s) capable of opening the required orifice size at a specific pressure (and specific gravity if other than cold water—specific gravity 1.0).

NOTE: If specific gravity falls between those shown in the tables, use next lower. Example: If specific gravity is 0.73, use 0.70 gravity data.

Safety Factors

Safety factor is the ratio between actual continuous discharge capacity of the drain trap and the amount of liquid to be discharged during any given period. Chart LD-12 shows the maximum continuous rate of cold water discharge of the drain trap. However, you must provide capacity for peak loads and, possibly, lower-than-normal pressures. A safety factor of 1-1/2 or 2 is generally adequate if applied to the peak load and the minimum pressure at which it occurs. If the load discharge to the trap is sporadic, a higher safety factor may be required. Contact your Armstrong Representative for details.

Selection Examples

EXAMPLE No. 1: Find a drain trap to drain 1 000 lbs of water per hour from air at 500 psig pressure differential.

Multiply 1 000 lbs/hr by 2 (if not already done) to provide a safety factor; thus, a 2 000 lbs/hr continuous discharge capacity is required. In Capacity Chart LD-12, the 2 000 lb capacity line intersects the 500 psig pressure line directly below the No. 38 drill orifice curve. This orifice is available in the No. 1-LD or No. 11-LD drain trap, but for much lower pressures. Moving to the 32-LD, a #38 orifice is good to 489 psig. This is the trap/orifice combination to use.

Table LD-14, page LD-37, shows the No. 32-LD drain trap with #38 orifice will operate at pressures up to 489 psig and, therefore, is suitable for the job. Further checking shows the No. 2313 HLS drain trap with a 7/64" orifice could also handle the job, but it is designed particularly for low gravity liquids and is more costly than the No. 32-LD, so the No. 32-LD is a better choice.

EXAMPLE No. 2: Find a drain trap to drain 6 400 lbs/hr (safety factor included) of .80 specific gravity liquid from gas at 400 psig pressure differential.

Since Capacity Chart LD-12 is based on water capacity, the known light liquid capacity requirement must be converted to its equivalent water capacity with the factor given in Table LD-5: $6\,400 \times 1.12 = 7\,168$ = water capacity required for using Chart LD-12.

Chart LD-12 shows that 7 168 lbs/hr and 400 psig calls for a 7/32" orifice. Entering the .80 specific gravity column of Table LD-14, page LD-37, shows that a No. 36-LD forged steel drain trap will open a 7/32" orifice at pressures up to 707 psig. As a matter of fact, this drain trap will open a 1/4" orifice at 501 psig and would be the one to use.

NOTE: While drain traps are sized on the basis of pressure differential, steel must be used whenever gauge pressure in the drain trap exceeds 250 psig.

Where Not to Use

Float type drain traps are not recommended where heavy oil, sludge or considerable dirt are encountered in lines. Dirt can prevent the valve from seating tightly, and cold oil can prevent float traps from opening. Where these conditions exist, Armstrong inverted bucket BVSF traps should be used.

How to Order Drain Traps

Specify:

- Drain trap size by number
- Orifice size
- Pipe connections—size and type
- Maximum operating pressure

If the correct drain trap cannot be determined, tell us capacity required, maximum pressure, and SPECIFIC GRAVITY of liquid.

Table LD-5. Conversion Factors to Find Cold Water Capacity Equivalents for Light Liquids

Specific Gravity	Multiply Light Liquid Capacity in Pounds Per Hour by:
.95	1.03
.90	1.06
.85	1.09
.80	1.12
.75	1.16
.70	1.20
.65	1.24
.60	1.29
.55	1.35
.50	1.42
.45	1.49
.40	1.58

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How to Select and Size Armstrong Drain Traps

For Draining Water From a Light Liquid

Armstrong dual gravity drain traps for draining water from a light liquid are described on pages LD-47 and LD-48. All models shown are identical to corresponding models of traps used to drain liquid from a gas except that float weights are modified to make them suitable for draining water from a light liquid.

Dual gravity drain trap* selection requires that you know the peak heavy liquid load, maximum operating pressure, and specific gravity of the light liquid. With this information you can determine the orifice size required from Chart LD-12 and find the specific drain trap that will meet your conditions from the pressure tables on the dual gravity pages.

Selection Procedure for Draining Water from a Light Liquid

1. Assume a required safety factor of 2:1. Multiply the peak load in pounds per hour by 2. (See paragraph on "Safety Factors.")
2. From Capacity Chart LD-12, find the intersection of actual load times safety factor and the minimum operating pressure differential. Follow the pressure line immediately above this point to intersect the next higher orifice capacity curve. Then follow this curve downward and to the left to get the orifice size.
3. Inspect the tables on pages LD-47 and LD-48 to find the smallest trap that can open the predetermined orifice size at the maximum operating pressure differential. Do not oversize dual gravity drain traps. Oversizing will cause excessive fluctuation of the interface between the two liquids.

NOTE: While drain traps are sized on the basis of operating pressure differential, forged steel must be used when total pressure in the drain trap exceeds 250 psig.

How to Order Dual Gravity Drain Traps

Specify:

- Drain trap size by number
- Orifice size
- Pipe connections—size and type
- Specific gravity of light liquid
- Weight of water discharge per hour
- Maximum operating pressure

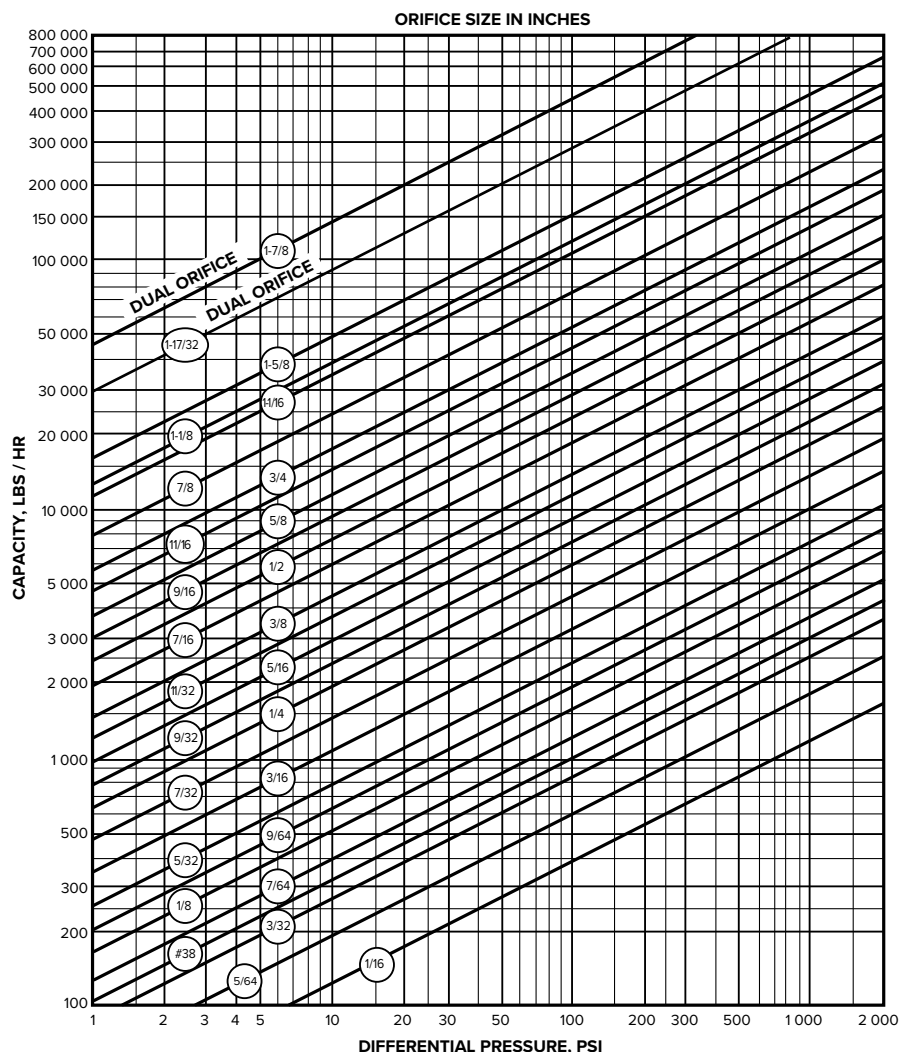
If you are not sure of the drain trap size to use, then specify:

- Specific gravity of light liquid
- Capacity in pounds of water per hour with safety factor included
- Working pressure—maximum and minimum

Chart LD-12.

Calculated Cold Water Capacity of Armstrong Drain Trap Orifices at Various Pressures

Actual capacity also depends on trap configuration, piping and flow to trap. It is important to allow for safety factors and fluid density variations due to temperature.



* Floats for dual gravity drain traps are weighted with quenching oil which, in the unlikely possibility of float failure, may be dispersed through the system. If this is a hazard, consult the Armstrong Application Engineering Department.



1-LDC—A See-Thru Body So You'll Know When It's Working

Benefits You Can See

Reduced maintenance
Stainless steel internals mean corrosion resistance and reduced maintenance.

Efficient operation
Simple ball float mechanism discharges only when liquid is present so it doesn't waste air.

Positive seating
Free-floating valve mechanism assures positive seating so it prevents air loss. There are no fixed pivots to wear or create friction, and wear points are heavily reinforced for long life.

An inside look
See-thru body means you can observe changing conditions as they occur. See a problem in the making—instead of having to deal with it after the fact.

In-line repairability
In-line connections and an O-ring seal make for quick, easy repairs without dismantling piping. Just unscrew and remove the body for maintenance.

Corrosion resistance
Long-lasting polycarbonate body and reinforced nylon cap weigh less than 20% of cast iron liquid drain traps. Rugged polysulfone resists corrosion and provides long, trouble-free service life.

Reduced need for cleaning
Recessed dirt pocket gives dirt a place to accumulate away from the valve seat. Valve seat is 1-1/4" above the dirt pocket. Compared to other ball float drain traps, the Armstrong 1-LDC reduces dirt fouling and needs less frequent cleaning.

Simplified installation
Optional horizontal or vertical inlet with horizontal outlet eliminates the need for extra fittings. Makes installation in existing systems easier. Vertical inlet is 3/4" to accommodate air venting. Requires no electricity.

NOTE: The Armstrong 1-LDC is not recommended for extremely dirty systems or those with heavy oil carryover. The drain trap should not be used in an environment where there are high levels of ketones or chlorinated or aromatic hydrocarbons.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

1-LDC—A See-Thru Body So You'll Know When It's Working

Now, you can literally see what you've been missing—the early warning signs of a drain trap or system problem. Since you'll know the operating condition of a drain trap, you won't waste time and money scheduling maintenance that isn't needed. In other words, you will be able to react to a condition before it becomes a problem.

A simple ball float mechanism requiring no electricity to operate, the new Armstrong 1-LDC discharges automatically only when liquid is present. That means no air loss as with timed devices, which open even when liquid is not present.

Moisture in a compressed air system causes a variety of problems— everything from dirt fouling and potential corrosion to water hammer. Getting the water out—automatically, reliably—builds greater efficiency into your system. In short, pay attention to your compressed air system, and you'll probably pay less to compress air.

Compare...and Save the Difference

Seeing really is believing—especially when you compare the Armstrong see-thru drain trap with cast iron units. Measure the differences in the time and money you can save with a more efficient, easier-to-maintain compressed air system. For more information or technical assistance, contact your local Armstrong Representative.



1-LDC See-Thru Liquid Drainer

For Loads to 1 500 lb/hr (690 kg/hr)...Pressures to 150 psig (10 barg)

Now, you can literally see what you've been missing—the early warning signs of a drain trap or system problem. Since you'll know the operating condition of a drain trap, you won't waste time and money scheduling maintenance that isn't needed. In other words, you'll be able to react to a condition before it becomes a problem.

A free floating mechanism needs no electricity to operate, the 1-LDC discharges automatically only when liquid is present. That means no air loss as with timed devices that open even when liquid is not present. Moisture in a compressed air system causes problems. Getting the water out—automatically, reliably—builds greater efficiency into your system.

List of Materials

Table LD-6.	
Name of Part	Material
Cap and Fitting	Reinforced Nylon*
Body	Polycarbonate
O-Rings (Cap, Body and Fitting)	Nitrile Elastomer Compound
Float, Lever and Screws	Stainless Steel
Valve & Seat	
Retainer Ring	Zinc-Plated Steel

*UV sensitive

Maximum Operation Pressures and Capacities

Table LD-7.		1.0				0.95			
Specific Gravity									
Orifice Size	Maximum Operating Pressure	Capacity		Maximum Operating Pressure		Capacity			
	psig	barg	lb/hr	kg/hr	psig	barg	lb/hr	kg/hr	
1/8	121	8.3	1 500	690	109	7.6	1 400	640	
#38	150	10.0	1 100	510	150	10.0	1 100	490	

Capacities given are continuous discharge capacities in lb/hr or kg/hr of liquid at pressure differential indicated.

Physical Data

Table LD-8.		
Inlet Connections	in	mm
	1/2, 3/4	15, 20
Outlet Connection	1/2	15
Alternate Inlet or Vent Connection	1/2, 3/4	15, 20
"A"	3-1/2	89
"B"	6-7/8	175
"C"	6-3/32	155
Weight lbs (kg)	1 (0.45)	
Maximum Allowable Pressure (Vessel Design)	150 psig @ 150°F (10 barg @ 65°C)	
Maximum Operating Pressure psig (barg)	150 (10)	

How to Order

Body Inlet ①	Cap Inlet ②	Cap Outlet ③
3/4"	1/2"	1/2"
1/2" or 3/4"	1/2" or 3/4"	1/2"

For a fully detailed certified drawing, contact Armstrong.

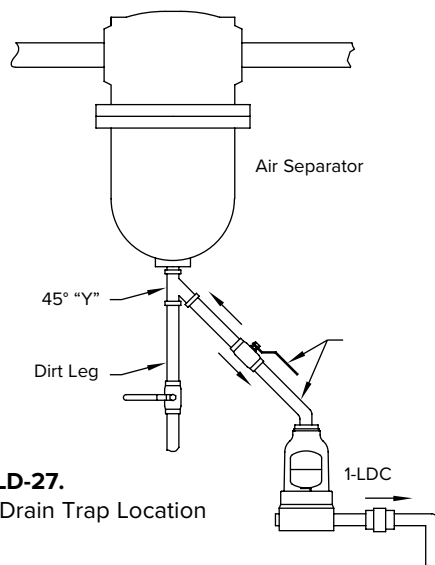
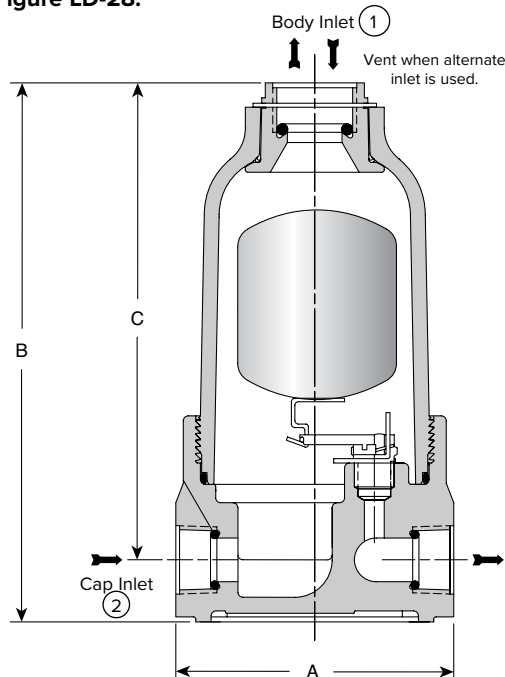


Figure LD-27.
Typical Drain Trap Location

Drain traps dispose of water that collects in many places in a compressed air system. Each drain trap arrangement must be considered individually.

Figure LD-28.



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

1-LDCW See-Thru Air Liquid Drainer for Ozone Applications

For Pressures to 150 psig (10 barg) or Specific Gravity 1.0

What Is Ozone?

Ozone is a gas that forms naturally during thunderstorms when lightning converts normal oxygen molecules (O_2) into ozone (O_3). The fresh, sweet smell in the air after a storm is the smell of ozone. The unstable ozone molecule reacts rapidly with most substances and is an extremely strong natural oxidant.

How Is Commercial Ozone Produced?

Ozone can be formed by exposing air to ultraviolet light; however, the most common method of generating ozone is by passing air through an electrical discharge. Because ozone has strong oxidizing properties, its production requires corrosion-resistant equipment.

How Is Ozone Used in Water Filtration and Purification?

Because ozone is such an effective oxidant, it kills viruses, bacteria, mold, mildew, fungus and germs. Passing ozone through water achieves high purification rates without any chemical residue. Oxygen is the only by-product.

Typical Customer Applications:

- Purifying standing ground water in Third World countries.
- Conditioning water for poultry and livestock.
- Purifying water in the bottled water industry.
- Filtering and purifying water for process applications.

A See-Thru Body Shows You It's Working

Now, you can literally see what you've been missing. The Armstrong 1-LDCW See-Thru Liquid Drainer lets you easily check its operating condition. You won't have to waste time and money scheduling maintenance that isn't needed, and you can quickly react to a condition before it becomes a problem.

Efficient Operation

Simple ball-float mechanism doesn't need electricity to operate. The liquid drainer automatically discharges liquid when it is present. No air or gas is lost, as with manual draining.

Positive Seating

Free-floating valve mechanism ensures positive seating and prevents liquid loss. There are no fixed pivots to wear or create friction. Wear points are heavily reinforced for long life.

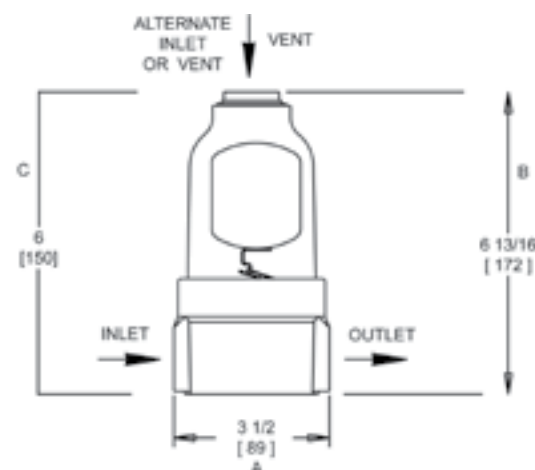
Corrosion Resistance

Long-lasting polycarbonate cap and body provides trouble-free operation. T316 stainless steel internal parts resist corrosion and reduce maintenance.

Compare—and Save the Difference

Seeing really is believing—especially when you compare the Armstrong 1-LDCW See-Thru Air Liquid Drainer with manual drainage. Measure the time and money you can save with a more efficient, easier-to-maintain system. For more information or technical assistance, contact your local Armstrong Representative.

NOTE: The Armstrong 1-LDCW should not be used in an environment where there are high levels of ketones or chlorinated or aromatic hydrocarbons.



1-LDCW

List of Materials	
Name of Part	Material
Cap	Polycarbonate
Body	Polycarbonate
O-Rings (Body Cap and Fitting)	Aflas
Float Lever and Screws	T316 Stainless Steel
Valve & Seat	T316 Stainless Steel
Fitting	Polycarbonate
Retainer Ring	Zinc Plated Steel

Physical Data		
	in	mm
Inlet Connection (In Body)	3/4	20
Inlet Connection (Alternate)	1/2	15
Outlet Connection	1/2	15
"A" Face-to-Face	3-1/2	89
"B" Height	6-13/16	172
"C" Bottom to C	6	152
Maximum Allowable Pressure (Vessel Design)	150 psig @ 150°F (10 barg @ 66°F)	
Maximum Operating Pressure	150 psig (10 barg)	
Specific Gravity Range	1.00 to 0.80	
Weight, lb (kg)	1 (.5)	

Inverted Bucket Drain Traps (BVSW Model)

For Loads to 7 000 lb/hr (3 175 kg/hr)...Pressures to 650 psig (45 barg)

Armstrong inverted bucket drain traps are designed for systems where heavy oil and dirt may be encountered. The enlarged bucket vent equipped with a scrub wire (BVSW) keeps the drain trap operating under dirty conditions.

List of Materials

Table LD-9.				
BVSW Model No.	Body & Cap	Valve & Seat	Bucket & Leverage System	Gasket
800, 811, 812, 813, 880, 881, 882, 883, 211, 212, 213	Cast Iron ASTM A48 Class 30	Stainless Steel		Compressed Asbestos-free
312, 313	Forged Steel ASTM A105			
971, 973	ASTM 216 Grade WCB (Body) / ASTM A351 Gr. CF8M (Cap)			



Physical Data

Table LD-10. Orifices, Maximum Operating Pressure (See Chart LD-12, page LD-30, for cold water capacities at various pressures.)												
Model No.	800 BVSW 880 BVSW		811 BVSW 881 BVSW 211 BVSW		812 BVSW 882 BVSW 212 BVSW		312 BVSW*		813 BVSW 883 BVSW 213 BVSW 313 BVSW* 973 BVSW*		971 BVSW*	
Orifice Size												
in	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
1/4	—	—	—	—	—	—	—	—	125	8.4	—	—
7/32	—	—	—	—	—	—	—	—	180	12.4	—	—
3/16	—	—	—	—	—	—	—	—	250	17.2	50	3.5
5/32	—	—	—	—	125	8.5	—	—	450	31	85	6
1/8	80	5.5	125	8.5	200	14	—	—	600	41.3	175	12
7/64	125	8.5	200	14	250	17	600	41	—	—	250	17
#38	150	10.5	250	17	—	—	—	—	—	—	325	22.4

NOTE: Larger capacity models available. Consult your local Armstrong Representative or the Armstrong factory.

* Use steel traps for pressures above 250 psig (17 barg).

Table LD-11. Armstrong 800 Series Drain Traps								
Model No.	800 BVSW		811 BVSW		812 BVSW		813 BVSW	
Pipe Connections	in	mm	in	mm	in	mm	in	mm
	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4	15, 20	3/4, 1	20, 25
Test Plug	1/4	6	1/4	6	1/2	15	3/4	20
“A”	3-3/4	95	3-3/4	95	5-5/8	143	7	178
“B”	5-7/16	138	6-7/8	175	9-1/16	230	11-3/4	298
“C”	5	127	5	127	6-1/2	165	7-3/4	197
“D”	2-3/4	70	4-1/4	108	5-3/8	137	7-1/32	179
Number of Bolts	6		6		6		6	
Weight lbs (kg)	5 (2.3)		6 (2.7)		15 (6.8)		27-1/2 (13)	
Maximum Allowable Pressure (Vessel Design)	250 psig @ 450°F (17 barg @ 232°C)							
Max. Operating Pressure psig (barg)	150 (10.5)		250 (17)					

NOTE: Larger capacity models available. Consult your local Armstrong Representative or the Armstrong factory.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Inverted Bucket Drain Traps (BVSW Model)

For Loads to 7 000 lb/hr (3 175 kg/hr)...Pressures to 650 psig (45 barg)



Physical Data

Table LD-12. Armstrong 880-970 Series Drain Traps With Integral Strainers (See pages LD-29 and LD-30 for capacity.)												
Model No.	Cast Iron								Cast Steel			
	880 BVSW		881 BVSW		882 BVSW		883 BVSW		971 BVSW		973 BVSW	
Pipe Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4	15, 20	3/4, 1, 1-1/4	20, 25, 32	1/2, 3/4, 1	15, 20, 25	3/4, 1	20, 25
Test Plug	1/4	6	1/4	6	1/2	15	3/4	20	—	—	—	—
“A”	3-3/4	95	3-3/4	95	5-5/8	143	7	178	4-11/16	119	7-7/16	188
“B”	6-1/16	154	7-1/16	179	9-3/8	244	12-3/8	314	9	229	12-15/16	328
“C”	5	127	5	127	6-1/2	165	7-7/8	200	6	152	8-1/8	206
“D”	3-7/16	87.3	4-7/16	113	5-3/4	146	7-3/8	187	5-7/16	138	7-1/2	190
Number of Bolts	6		6		6		6		6		6	
Weight lbs (kg)	5-1/2 (2.5)		6 (2.7)		15-1/2 (7)		31 (14)		15 (6.8)		44 (20)	
Maximum Allowable Pressure (Vessel Design)	250 psig @ 450°F (17 barg @ 232°C)								600 psig @ 650°F (41 barg @ 343°C)			
Max. Oper. Pressure psig (barg)	150 (10.5)		250 (17)						600 (41)		600 (41)	

NOTE: Larger capacity models available. Consult your local Armstrong Representative or the Armstrong factory.

Table LD-13. Armstrong 200-300 Series Drain Traps (See pages LD-29 and LD-30 for capacity.)										
Model No.	Cast Iron						Forged Steel			
	211 BVSW		212 BVSW		213 BVSW		312 BVSW		313 BVSW	
Pipe Connections	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2	15	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25
Test Plug	1/8	3	3/8	10	1/2	15	—	—	—	—
“A”	4-1/4	108	5-1/4	133	6-3/8	162	6-3/4	171	8	203
“B”	6-3/8	162	8-3/4	222	10-3/4	273	10-3/16	259	11-1/2	292
“G”	—	—	—	—	—	—	4-3/4	121	5-1/8	130
“K” (℄ Outlet to ℄ Inlet)	—	—	—	—	—	—	1-1/4	31.7	1-7/16	36.5
Number of Bolts	6		8		6		6		8	
Weight lbs (kg)	6 (2.7)		11-1/2 (5.2)		20-1/4 (9.2)		30 (14)		50 (23)	
Maximum Allowable Pressure (Vessel Design)	250 psig @ 450°F (17 barg @ 232°C)						600 psig @ 650°F (41 barg @ 343°C)		1 080 psig @ 650°F (75 barg @ 343°C)	
Max. Oper. Pressure psig (barg)	250 (17)						600 (41)		650 (45)	

NOTE: Larger capacity models available. Consult your local Armstrong Representative or the Armstrong factory.

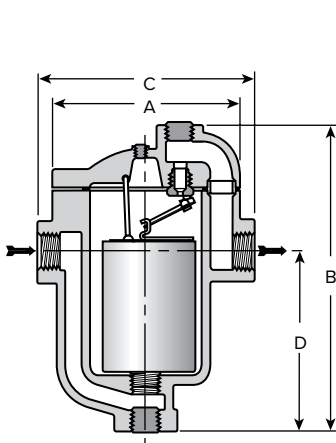


Figure LD-29.
Series 800

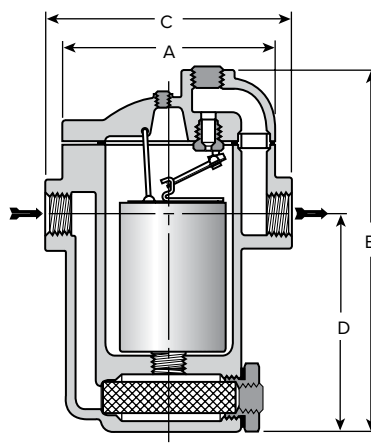


Figure LD-30.
Series 880 & 970

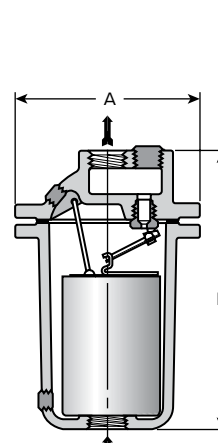


Figure LD-31.
Series 200

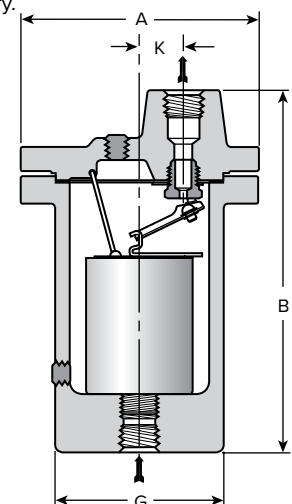


Figure LD-32.
Series 300

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Free Floating Lever Drain Traps

For Loads to 50 000 lb/hr (22 679 kg/hr)...Pressures to 1 000 psig (69 barg)

Table LD-14. Maximum Operating Pressures for Handling Different Specific Gravity Liquids With Orifices Available in Guided Free Floating Lever Drain Traps. (See pages LD-29 and LD-30.)

Model No.	Sp. Grav	1.00		.95		.90		.85		.80		.75		.70		.65		.60		.55		.50	
	Orifice	Maximum Operating Pressure psig (barg)																					
		in	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig
1-LD	1/8	121	8.3	109	7.6	98	6.8	87	6.0	75	5.2	64	4.4	52	3.6	41	2.8	29	2.0	18	1.2	6	0.4
	7/64	143	9.9	130	9.0	116	8.0	103	7.1	89	6.1	75	5.2	62	4.3	48	3.3	35	2.4	21	1.4	7	0.5
	#38	182	12.5	164	11	147	10.2	130	9.0	113	7.8	95	6.6	78	5.4	61	4.2	44	3.0	26	1.8	9	0.6
	5/64	300	20.7	289	19.9	259	17.8	228	15.7	198	13.7	168	11.6	137	9.5	107	7.4	77	5.3	47	3.2	16	1.1
11-LD	1/8	176	12.1	161	11.1	146	10.1	130	9.0	115	7.9	100	6.9	85	5.8	69	4.8	54	3.7	39	2.7	24	1.6
	7/64	209	14	191	13	173	12	155	10.7	137	9.4	119	8.2	100	6.9	82	5.7	64	4.4	46	3.2	28	1.9
	#38	264	18	242	17	219	15	196	14	173	12	150	10.4	127	8.8	104	7.2	81	5.6	59	4.0	36	2.5
	5/64	400	28	400	28	384	27	344	24	304	21	264	18	224	15	183	13	143	9.9	103	7.1	63	4.3
2-LD to 250 psig (17 barg)	5/16	22	1.5	20	1.4	18	1.3	17	1.1	15	1.0	13	0.9	11	0.8	10	0.7	8	0.5	6	0.4	4	0.3
	1/4	36	2.5	33	2.3	30	2.1	27	1.9	24	1.7	22	1.5	19	1.3	16	1.1	13	0.9	10	0.7	7	0.5
	3/16	79	5.5	73	5.0	67	4.6	60	4.2	54	3.7	47	3.3	41	2.8	35	2.4	28	2.0	22	1.5	16	1.1
	5/32	137	9.4	126	8.7	115	7.9	104	7.2	93	6.4	82	5.6	71	4.9	60	4.1	49	3.4	38	2.6	27	1.8
22-LD to 533 psig (37 barg)	1/8	234	16.1	215	14.8	196	13.5	178	12.2	159	10.9	140	9.6	121	8.4	102	7.1	83	5.8	65	4.5	46	3.2
	7/64	299	20.6	275	19	251	17.3	227	15.7	203	14	179	12	155	10.7	131	9.0	107	7.4	83	5.7	59	4.0
	#38	372	25.7	342	23.6	313	21.6	283	19.5	253	17.4	223	15	193	13	163	11.2	133	9.2	103	7.1	73	5.0
	5/64	533	37	475	33	461	32	417	29	372	26	328	23	284	20	240	17	196	14	152	10.5	108	7.4
32-LD	5/16	29	2.0	26	1.8	23	1.6	21	1.4	18	1.2	15	1.0	12	0.9	10	0.7	7	0.5	4	0.3	2	0.1
	1/4	47	3.3	43	3.0	38	2.6	34	2.3	29	2.0	25	1.7	20	1.4	16	1.1	12	0.8	7	0.5	3	0.2
	3/16	104	7.2	94	6.5	85	5.8	75	5.2	65	4.5	55	3.8	45	3.1	35	2.4	25	1.8	16	1.1	6	0.4
	5/32	180	12	163	11	146	10	129	8.9	112	7.7	95	6.5	78	5.4	61	4.2	44	3.0	27	1.9	10	0.7
3-LD to 250 psig (17 barg) (Cast Iron)	1/8	307	21	278	19	249	17	220	15	191	13	162	11	133	9	104	7.2	75	5.2	46	3.2	17	1.2
	7/64	393	27	356	25	319	22	282	19	245	17	207	14	170	12	133	9	96	6.6	59	4.1	22	1.5
	#38	489	34	443	31	397	27	351	24	304	21	258	18	212	15	166	11	120	8	73	5.1	27	1.9
	5/64	600	41	600	41	585	40	517	36	449	31	381	26	313	22	244	17	176	12	108	7	40	2.8
13-LD to 570 psig (39 barg) (Stainless)	1/2	16	1.1	14	1.0	13	0.9	12	0.8	10	0.7	9	0.6	7	0.5	6	0.4	5	0.3	3	0.2	2	0.1
	3/8	33	2.3	31	2.1	28	1.9	25	1.7	22	1.5	19	1.3	16	1.1	13	0.9	10	0.7	7	0.5	4	0.3
	5/16	54	3.7	49	3.4	44	3.0	39	2.7	35	2.4	30	2.1	25	1.7	20	1.4	16	1.1	11	0.8	6	0.4
	9/32	71	4.9	65	4.5	59	4.0	52	3.6	46	3.2	40	2.7	34	2.3	27	1.9	21	1.4	15	1.0	8	0.6
33-LD to 900 psig (62 barg) (Steel)	1/4	107	7.4	97	6.7	88	6.1	79	5.4	69	4.8	60	4.1	50	3.5	41	2.8	32	2.2	22	1.5	13	0.9
	7/32	153	10.5	139	9.6	126	8.7	112	7.7	99	6.8	85	5.9	72	5.0	59	4.0	45	3.1	32	2.2	18	1.2
	3/16	230	16	209	14	189	13	169	12	149	10.3	129	8.9	108	7.5	88	6.1	68	4.7	48	3.3	27	1.9
	5/32	359	25	327	23	296	20	264	18	233	16	201	14	169	12	138	9.5	106	7.3	74	5.1	43	2.9
6-LD Cast Iron	1/8	726	50	662	46	598	41	534	37	470	32	406	28	342	24	278	19	214	15	150	10.3	86	5.9
	7/64	900	62	847	58	765	53	683	47	601	41	519	36	437	30	356	25	274	19	192	13	110	7.6
	1-1/16	21	1.4	19	1.3	18	1.2	16	1.1	15	1.0	13	0.9	12	0.8	10	0.7	9	0.6	7	0.5	6	0.4
	7/8	32	2.2	30	2.1	28	1.9	26	1.8	23	1.6	21	1.4	19	1.3	16	1.1	14	1.0	12	0.8	9	0.6
36-LD Forged Steel	3/4	47	3.2	44	3.0	40	2.8	37	2.5	34	2.3	30	2.1	27	1.9	24	1.6	20	1.4	17	1.2	14	0.9
	5/8	72	4.9	67	4.6	61	4.2	56	3.9	51	3.5	46	3.2	41	2.8	36	2.5	31	2.1	26	1.8	21	1.4
	9/16	95	6.5	88	6.1	81	5.6	75	5.2	68	4.7	61	4.2	55	3.8	48	3.3	41	2.8	34	2.4	28	1.9
	1/2	138	9.5	128	8.8	118	8.1	108	7.5	99	6.8	89	6.1	79	5.4	69	4.8	59	4.1	50	3.4	40	2.8
3-LD to 250 psig (17 barg) (Cast Iron)	7/16	196	13	182	13	168	12	154	11	140	10	126	8.7	112	7.7	98	6.8	85	5.8	71	4.9	57	3.9
	3/8	250	17	250	17	250	17	243	17	221	15	199	14	177	12	155	11	133	9.0	111	7.7	90	6.2
	11/32	250	17	250	17	250	17	250	17	250	17	250	17	250	17	236	16	207	14	178	12	148	10
	5/16	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	228	16	191	13
6-LD Cast Iron	9/32	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17
	1/4	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17
	7/32	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17
	3/16	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17	250	17
36-LD Forged Steel	1-1/16	16	1.1	15	1.01	13	0.91	12	0.81	10	0.71	9	0.6	7	0.5	6	0.4	4	0.3	3	0.2	1	0.1
	7/8	25	1.7	23	1.6	21	1.4	18	1.3	16	1.1	14	0.95	11	0.79	9	0.63	7	0.47	5	0.31	2	0.16
	3/4	36	2.5	33	2.3	30	2.1	27	1.8	23	1.6	20	1.4	17	1.1	13	0.91	10	0.68	7	0.45	3	0.22
	5/8	56	3.9	51	3.5	46	3.1	41	2.8	35	2.4	30	2.1	25	1.7	20	1.4	15	1.05	10	0.69	5	0.34
3-LD to 250 psig (17 barg) (Cast Iron)	9/16	74	5.1	67	4.6	60	4.2	54	3.7	47	3.2	40	2.8	34	2.3	27	1.8	20	1.4	13	0.92	7	0.46
	1/2	107	7.4	97	6.7	88	6.0	78	5.4	68	4.7	58	4.0	49	3.4	39	2.7	29	2.0	19	1.3	10	0.66
	7/16	152	10.5	138	9.6	125	8.6	111	7.6	97	6.7	83	5.7	69	4.8	55	3.8	41	2.9	27	1.9	14	0.94
	3/8	240	17	218	15	197	14	175	12	153	10.5	131	9.0	109	7.5	87	6.0	65	4.5	43	3.0	21	1.5
6-LD Cast Iron	11/32	320	22	291	20	262	18	233	16	203	14	174	12	145	10	116	8.0	87	6.0	58	4.0	29	2.0
	5/16	411	28	374	26	336	23	299	21	262	18	224	15	187	13	149	10.3	112	7.7	74	5.1	37	2.5
	9/32	539	37	490	34	441	30	392	27	343	24	293	20	244	17	195	13	146	10.1	97	6.7	48	3.3
	1/4	788	54	716	49	644	44	573	39	501	35	429	30	357	25	286	20	214	15	142	9.8		

Free Floating Lever Drain Traps

For Loads to 49 000 lb/hr (22 226 kg/hr)...Pressures to 300 psig (21 barg)

Armstrong's cast iron, free floating lever drain traps use the same bodies, caps, lever mechanisms, valves and seats of Armstrong inverted bucket steam traps that have been proven in years of service. Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for drain trap size and weight.

The hemispherical valve, seat and leverage of the 1-LD, 2-LD, 3-LD and 6-LD cast iron traps are identical in design, materials and workmanship to those for saturated steam service up to 300 psig (21 barg) with the exception of the addition of a guidepost to assure a positive, leaktight valve closing under all conditions.

List of Materials

Table LD-15.					
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
1-LD 2-LD 3-LD 6-LD	Stainless Steel			Cast Iron ASTM A48 Class 30	Compressed Asbestos-free

For information on special materials, consult the Armstrong Application Engineering Department.

For a fully detailed certified drawing, refer to:

1-LD CD #1070

2-LD, 3-LD, 6-LD CD #1034

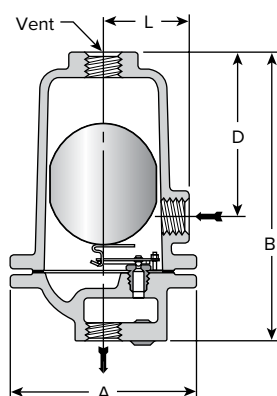


Figure LD-33.

No. 2-LD, 3-LD and 6-LD cast iron guided lever drain traps. No. 1-LD has standard top inlet and optional side connection.



Physical Data

Table LD-16. Armstrong Guided Lever Liquid Drain Traps								
Model No.	Cast Iron							
	1-LD		2-LD		3-LD		6-LD	
Pipe Connections	in	mm	in	mm	in	mm	in	mm
	1/2*	15*	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1-1/2, 2	40, 50
"A"	3-3/4	95	5-1/4	133	6-3/8	162	10-3/16	259
"B"	5-1/2	140	8-3/4	222	11-1/2	292	18	457
"D"	2-7/8	73	5-1/8	130	7	188	9-3/8	238
"K" (℄ Outlet to ℄ Inlet)	13/16	21	—	—	—	—	—	—
"L"	1-7/8	48	2-7/16	62	2-7/8	73	4-5/8	117
Approx. Wt. lb (kg)	4 (2)		12 (5.5)		21 (9.5)		78 (35.5)	
Max. Allow. Pressure (Vessel Design)	300 psig @ 200°F† (21 barg @ 93°C)		250 psig @ 450°F (17 barg @ 232°C)					

NOTE: Vessel design pressure may exceed float collapse pressure in some cases.

Pipe size of vent connection is same as that of inlet and outlet connections.

†For pressures not exceeding 250 psig (17 barg), a maximum temperature of 450°F (232°C) is allowed.

*1/4" (6 mm) outlet.

Free Floating Lever Drain Traps

For Loads to 9 500 lb/hr (4 309 kg/hr)...Pressures to 570 psig (39 barg)

Armstrong's stainless steel, free floating lever drain traps use the same bodies, caps, lever mechanisms, valves and seats of Armstrong inverted bucket steam traps that have been proven in years of service. Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for drain trap size and weight.

The hemispherical valve, seat and leverage of the 11-LD, 22-LD and 13-LD stainless steel traps are identical in design, materials and workmanship to those for saturated steam service up to 570 psig (39 barg) with the exception of the addition of a guidepost to assure a positive, leaktight valve closing under all conditions.

List of Materials

Table LD-17.

Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
11-LD 22-LD 13-LD	Stainless Steel*			Sealed Stainless Steel, 304L*	—

*11-LD available in all-316SS. Consult factory.

For information on special materials, consult the Armstrong Application Engineering Department.

For a fully detailed certified drawing, refer to list below:

11-LD CD #1066

13-LD and 22-LD CD #1086

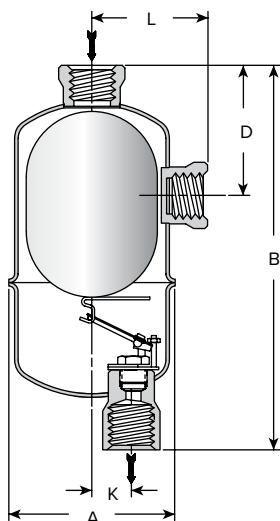


Figure LD-34.

No. 22-LD and 13-LD stainless steel guided lever liquid drain trap with sealed, tamperproof construction.



Physical Data

Table LD-18. Armstrong Guided Lever Liquid Drain Traps

Model No.	Stainless Steel					
	11-LD**		22-LD		13-LD	
Pipe Connections	in	mm	in	mm	in	mm
	3/4*	20*	3/4	20	1	25
"A"	2-3/4	70	3-15/16	100	4-1/2	114
"B"	7-1/4	184	8-13/16	224	11-3/8	289
"D"	—	—	3	76	6-1/8	156
"K"	9/16	14	7/8	22	1-3/16	30
"L"	—	—	2-5/8	67	3-9/32	83
Approx. Wt. lbs (kg)	1-3/4 (0.79)		3-1/4 (1.5)		7-1/2 (3.4)	
Max. Allowable Pressure (Vessel Design)	500 psig @ 100°F (35 barg @ 38°C) 440 psig @ 500°F (30 barg @ 260°C)		600 psig @ 100°F (41 barg @ 38°C) 475 psig @ 500°F (33 barg @ 260°C)		570 psig @ 100°F (39 barg @ 38°C) 490 psig @ 500°F (34 barg @ 260°C)	

Note: Vessel design pressure may exceed float collapse pressure in some cases.

Pipe size of vent connection is same as that of inlet and outlet connections.

*1/2" (15 mm) outlet. **No side connection.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Free Floating Lever Drain Traps

For Loads to 42 000 lb/hr (19 050 kg/hr)...Pressures to 1 000 psig (69 barg)

Armstrong's forged steel, free floating lever drain traps use the same bodies, caps, lever mechanisms, valves and seats of Armstrong inverted bucket steam traps that have been proven in years of service. Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for drain trap size and weight.

The hemispherical valve, seat and leverage of the 32-LD, 33-LD and 36-LD forged steel traps are identical in design, materials and workmanship to those for saturated steam service up to 1 000 psig (69 barg) with the exception of the addition of a guidepost to assure a positive, leaktight valve closing under all conditions.

List of Materials

Table LD-21.

Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
32-LD 33-LD 36-LD	Stainless Steel			Forged Steel ASTM A105	Compressed Asbestos-free

For information on special materials, consult the Armstrong Application Engineering Department.

For a fully detailed certified drawing, refer to CD #1035.

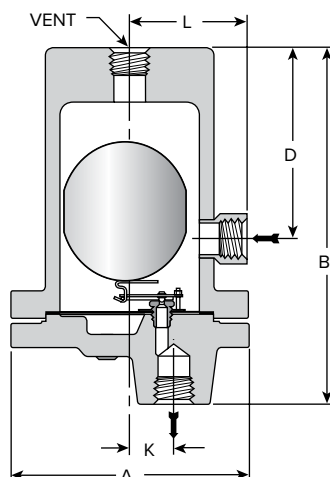


Figure LD-37.

No. 32-LD, 33-LD and 36-LD forged steel guided lever drain trap. Socketweld or flanged connections are also available.



Physical Data

Table LD-22. Armstrong Guided Lever Liquid Drain Traps

Model No.	Forged Steel					
	32-LD [†]		33-LD [†]		36-LD [†]	
Pipe Connections	in	mm	in	mm	in	mm
	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25	1-1/2, 2	40, 50
"A"	6-3/4	171	8	203	11-7/8	302
"B"	10-3/16	259	11-9/16	294	17-1/8	435
"D"	5-9/16	141	6-1/16	154	9	229
"K"	1-1/4	32	1-7/16	37	2-1/8	54
"L"	3-3/8	86	3-9/16	90	6-1/16	154
Approx. Wt. lbs (kg)	31 (14)		49 (22)		163 (74)	
Max. Allowable Pressure (Vessel Design)	600 psig @ 100°F (41 barg @ 38°C) 500 psig @ 750°F (35 barg @ 400°C)		1 000 psig @ 100°F (69 barg @ 38°C) 600 psig @ 750°F (41 barg @ 400°C)			

Note: Vessel design pressure may exceed float collapse pressure in some cases.

Pipe size of vent connection is same as that of inlet and outlet connections.

[†]Available in Type 316 stainless steel. Consult factory.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



180 Series Free Floating Lever Drain Traps

All Stainless Steel for Horizontal Installation

For pressures to 400 psig (28 barg) . . . Capacities to 2 000 lb/hr (907 kg/hr)

Armstrong's stainless steel, free floating lever drain traps use the same bodies, caps, lever mechanisms, valves and seats as Armstrong inverted bucket steam traps that have been proven in years of service. Elliptical floats and high leverage make it possible to open large orifices to provide adequate capacity for drain trap size and weight.

The hemispherical valve, seat and leverage of the 180-LD and 181-LD stainless steel traps are identical in design, materials and workmanship to those for saturated steam service up to 570 psig (39 barg), except that the 180 Series traps have a guidepost to ensure a positive, leak-tight valve closing under all conditions. The 180 Series is designed for situations where mounting a drainer close to the floor is critical. A back vent connection is required.

For a fully detailed certified drawing, refer to list below:
180-LD CD #1276

List of Materials

Table LD-19.

Model No.	Valve & Seat	Leverage System	Float	Body & Cap
180-LD 181-LD		Stainless Steel		Sealed Stainless Steel 304L

Physical Data

Table LD-20. Armstrong 180 Series Free Floating Lever Drain Traps

Model No.	180-LD		181-LD	
Pipe Connections	in	mm	in	mm
	1/2	15	3/4	20
"A" (Diameter)	2-11/16	68	2-11/16	68
"B" (Height)	6	152	7-1/4	184
"C" (Face to Face)	4-5/16	110	4-5/16	110
"D" (Bottom to C Inlet)	5-1/8	130	6-9/32	160
"P"	1/2	15	3/4	20
Weight, lb (kg)	1-3/4 (0.8)		2-3/8 (1.1)	
Max. Allowable Pressure (Vessel Design)	500 psig @ 100°F (35 barg @ 38°C) 440 psig @ 500°F (30 barg @ 260°C)			

Note: Vessel design pressure may exceed float collapse pressure in some cases. Pipe size of vent is same as that of inlet and outlet connections.

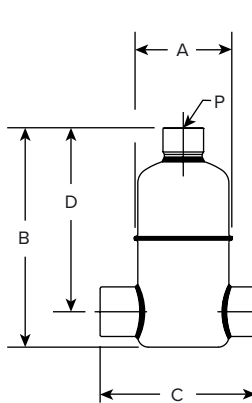


Figure LD-35.
Model 180-LD

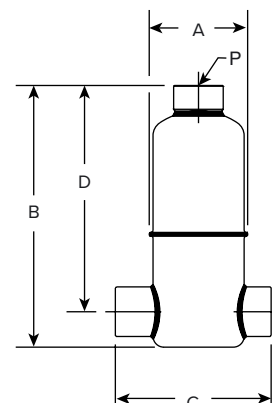


Figure LD-36.
Model 181-LD

Chart LD-13. Model 180-LD Capacity

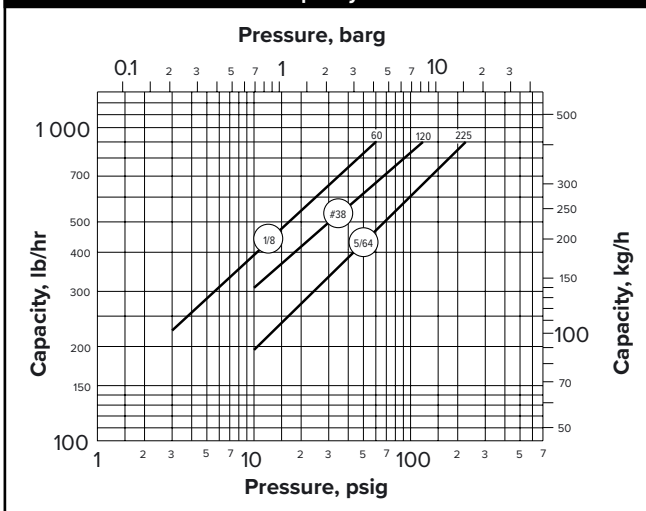
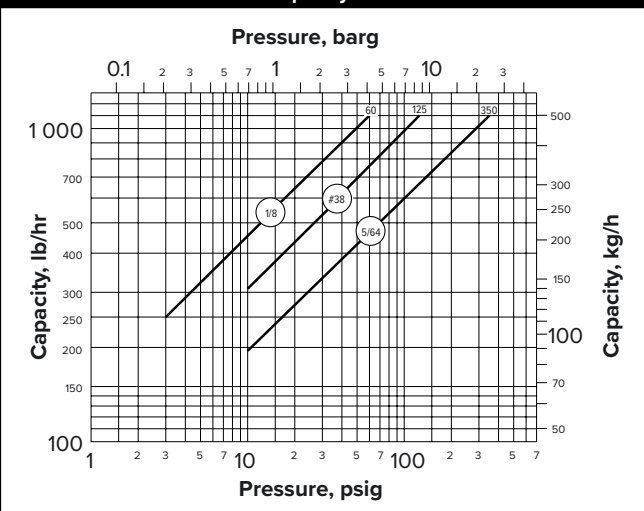


Chart LD-14. Model 181-LD Capacity



Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Notes

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Fixed Pivot and Snap Action Drain Traps

For Loads to 3 900 lb/hr (1 769 kg/hr)...Pressures to 1 000 psig (69 barg)

Continuous Flow or On-Off Float Type Drain Traps

Armstrong's line of fixed lever and snap action drain traps includes two basic models available in cast iron and forged steel. The floats are light enough to handle light liquids.

No. 21—A small, high-quality, economical drain trap for use on drainage jobs where dirt and oil are not encountered. It employs a single lever with a fixed pivot.

No. 21-312—Forged steel version of the No. 21 with larger float and higher leverage.

No. 71-A—Wide open, tight-shut drain trap for use where fine dirt and grit may be present or where liquid load is light. A flat spring in the leverage system holds the valve closed until the trap body is nearly full of water. Then it snaps open, washing dirt through. When the trap body is nearly empty, the spring snaps the valve shut.

No. 71-315—Forged steel version of No. 71-A.

CAUTION: Ball float drain traps are not recommended where heavy oil, sludge or considerable dirt are encountered in lines. Under these circumstances use Armstrong inverted bucket BWSV traps.

Table LD-23. Maximum Operating Pressures for Handling Different Specific Gravity With Orifices Available in Fixed Lever and Snap Action Drain Traps (See pages LD-29 and LD-30.)

Model No.		Sp. Grav.	1.00		.95		.90		.85		.80		.75		.70		.65		.60		.55		.50	
		Orifice size (in)	Maximum Operating Pressure psig (barg) at 100°F (38°C)																					
			psig	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig
21		1/4	22	1.5	20	1.4	18	1.3	16	1.1	15	1.0	13	0.9	11	0.8	10	0.7	8	0.5	6	0.4	4	0.3
		7/32	28	1.9	26	1.8	24	1.6	21	1.5	19	1.0	17	1.2	15	1.0	12	0.9	10	0.7	8	0.6	6	0.4
		3/16	38	2.6	35	2.4	32	2.2	29	2.0	26	1.8	23	1.6	20	1.4	17	1.2	14	1.0	11	0.7	8	0.5
		5/32	54	3.8	50	3.5	46	3.2	41	2.9	37	2.6	33	2.3	29	2.0	24	1.7	20	1.4	16	1.1	11	0.8
		9/64	67	4.6	62	4.2	56	3.9	51	3.5	46	3.1	40	2.8	35	2.4	30	2.1	24	1.7	19	1.3	14	1.0
		1/8	84	5.8	78	5.4	71	4.9	64	4.4	58	4.0	51	3.5	44	3.0	37	2.6	31	2.1	24	1.7	17	1.2
		3/32	148	10.2	136	9.4	124	8.6	112	7.7	101	6.9	89	6.1	77	5.3	66	4.5	54	3.7	42	2.9	30	2.1
		5/64	210	14	193	13	176	12	160	11	143	9.9	126	8.7	110	7.6	93	6.4	77	5.3	60	4.1	43	3.0
		1/16	250	17	250	17	250	17	245	17	220	15	194	13	168	12	143	9.9	117	8.1	92	6.3	66	4.6
21-312*	3-3/8 oz (96 g) Float	1/4	42	2.9	39	2.7	36	2.5	33	2.3	30	2.1	28	1.9	25	1.7	22	1.5	19	1.3	16	1.1	13	0.9
		7/32	54	3.8	51	3.5	47	3.2	43	3.0	40	2.7	36	2.5	32	2.2	28	2.0	25	1.7	21	1.5	17	1.2
		3/16	74	5.1	69	4.7	64	4.4	59	4.0	54	3.7	49	3.4	44	3.0	39	2.7	34	2.3	28	2.0	23	1.6
		5/32	200	14	197	14	182	13	168	12	153	10.6	139	9.6	125	8.6	110	7.6	96	6.6	82	5.6	67	4.6
	4-1/2 oz (128 g) Float	9/64	229	16	211	15	200	14	200	14	189	13	171	12	153	10.6	136	9.4	118	8.1	100	6.9	83	5.7
		1/8	288	20	266	18	243	17	221	15	200	14	200	14	193	13	171	12	148	10.2	126	8.7	104	7.2
		3/32	500	34	465	32	426	29	387	27	348	24	309	21	270	19	231	16	200	14	200	14	182	13
	6 oz (170 g) Float	5/64	589	41	533	37	500	34	500	34	495	34	440	30	384	27	329	23	274	19	218	15	200	14
1/16		600	41	600	41	600	41	600	41	563	39	500	34	500	34	500	34	420	29	335	23	250	17	
71-A & 71-315 **		1/4	10	0.7	10	0.7	10	0.7	10	0.7	10	0.7	10	0.7	10	0.7	10	0.7	—	—	—	—	—	—
		3/16	20	1.4	20	1.4	20	1.4	20	1.4	20	1.4	20	1.4	20	1.4	20	1.4	—	—	—	—	—	—
		1/8	100	6.9	100	6.9	100	6.9	100	6.9	100	6.9	100	6.9	100	6.9	100	6.9	—	—	—	—	—	—
		7/64	200	14	200	14	200	14	200	14	200	14	200	14	200	14	200	14	—	—	—	—	—	—
71-A		5/64	250	17	250	17	250	17	250	17	—	—	—	—	—	—	—	—	—	—	—	—	—	
71-315		5/64	500	35	500	35	500	35	500	35	—	—	—	—	—	—	—	—	—	—	—	—	—	
		1/16	1 000	69	1 000	69	1 000	69	1 000	69	—	—	—	—	—	—	—	—	—	—	—	—	—	

NOTE: If actual specific gravity falls between those shown in above table, use next lower. For example, if actual gravity is 0.73, use 0.70 gravity data.

*5/32" orifice (and smaller) utilizes higher leverage mechanism designated 21-312V.

**Use 6 1/4 oz. float for 0.85 - 1.0 S.G. Use 3 3/8 oz. float for 0.65 - 0.80 S.G.

Fixed Pivot and Snap Action Drain Traps

For Loads to 3 900 lb/hr (1 769 kg/hr)...Pressures to 1 000 psig (69 barg)



Physical Data

Table LD-24. Armstrong Fixed Lever and Snap Action Drain Traps								
Model No.	Cast Iron				Forged Steel			
	21 [†]		71-A*		21-312 [†]		71-315*	
Pipe Connections	in	mm	in	mm	in	mm	in	mm
	1/2, 3/4	15, 20	3/4, 1	20, 25	1/2, 3/4, 1	15, 20, 25	3/4, 1, 1-1/4, 1-1/2	20, 25, 32, 40
"A"	6-3/16	157	8-1/2	216	6-3/4	171	9-3/4	248
"B"	5-1/4	133	10-3/4	273	10-3/16	259	15-5/8	397
"D"	—	—	4-1/4	108	5-9/16	141	7-13/16	198
"K"	1-5/16	33	—	—	1-1/4	32	—	—
"L"	—	—	3-1/2	89	3-5/16	84	4-5/8	117
Weight, lbs (kg)	8 (4)		29 (13)		30 (14)		92 (42)	
Maximum Allowable Pressure (Vessel Design)	250 psig @ 450°F (17 barg @ 232°C)				600 psig @ 100°F (41 barg @ 38°C) 500 psig @ 750°F (34 barg @ 400°C)		1 000 psig @ 100°F (69 barg @ 38°C) 600 psig @ 750°F (41 barg @ 400°C)	

[†] Cast 316 stainless steel body and cap with all stainless steel internals available. Aluminum body and cap available for Model 21 only. Consult factory.

*Snap action drain traps should not be used where load exceeds 120 lb/hr (54 kg/hr). Use on greater loads shortens spring life.

List of Materials

Table LD-25.					
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
21	Stainless Steel			Cast Iron ASTM A48 Class 30	Compressed Asbestos-free
71-A				Forged Steel*	
21-312 71-315				ASTM A105	

*No. 71-315 cap is cast steel.

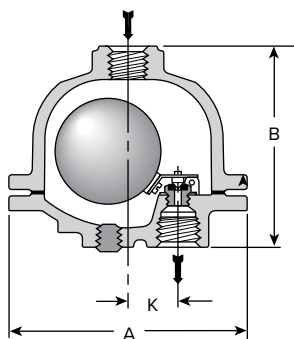


Figure LD-38.
No. 21 cast iron fixed lever drain trap.

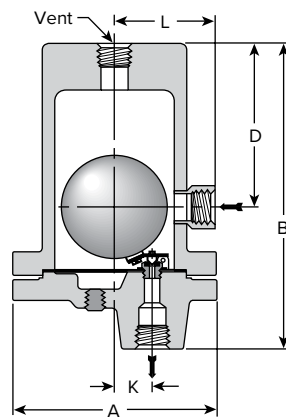


Figure LD-39.
No. 21-312 forged steel fixed lever drain trap.

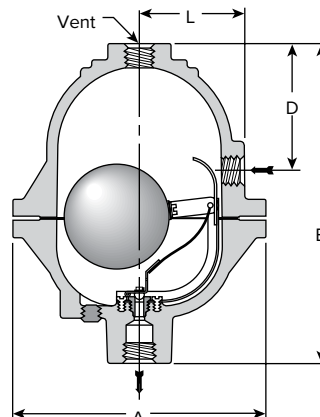


Figure LD-40.
No. 71-A cast iron snap action drain trap.

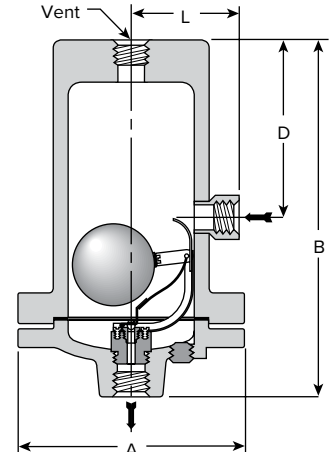


Figure LD-41.
No. 71-315 forged steel snap action drain trap.

For a fully detailed certified drawing, refer to list below:

No. 21	CD #1037	No. 71-A	CD #1038
No. 21-312	CD #1106	No. 71-315	CD #1107

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



High Leverage Spring-Loaded Ball Float Type Drain Traps

For Low Flows at Pressures to 3 700 psig (255 barg) and Specific Gravity Down to 0.40

The Armstrong High Leverage Series of liquid drain traps was developed especially for draining low specific gravity fluids from gases at high pressures. They use standard Armstrong forged steel bodies with very high leverage systems and spring assist.

NOTE: Models 2313-HLS, 2316-HLS, 2413-HLS and 2415-HLS are also available with cast T-316 stainless steel body and all-stainless steel internals. Consult factory.

Because of design considerations in this drain trap, it is essential that a safety factor of at least 2 be applied to the peak liquid load for sizing purposes.

Do not use HLS drain traps on steam service.

Sour Gas Service

Forged steel and stainless steel traps can be modified to resist hydrogen sulfide stress corrosion. These modifications involve annealing the float, which will reduce the maximum working pressure of the float to about half its normal value. Consult Armstrong Application Engineering for allowable working pressures.

Table LD-26. Reference Data

Model No.	Float Diameter	Unbalanced Float Weight
2313-HLS 2413-HLS 25133G-HLS	3-1/2" (89 mm)	4 oz (113 g)
2315-HLS 2415-HLS 25155G-HLS 26155G-HLS	4" (102 mm)	4-1/2 oz (128 g)
2316-HLS 2416-HLS	5" (127 mm)	6 oz (170 g)

Table LD-27. Maximum Operating Pressures for Handling Different Specific Gravity Liquids With Orifices Available in High Leverage Drain Traps (See pages LD-29 and LD-30.)

Model No.	Sp. Grav.	1.00		.95		.90		.85		.80		.75		.70		.65		.60		.55		.50		.45		.40			
	Orifice	Maximum Operating Pressure psig (barg) at 100°F (38°C)																											
	in	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg		
2313-HLS	1/16	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	630	43		
	5/64	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	940	65	670	47	410	29		
	3/32	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	850	58	660	46	480	33	290	20		
	7/64	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	910	63	770	53	630	44	490	34	360	25	220	15		
	1/8	1000	69	1000	69	1000	69	1000	69	1000	69	920	63	810	56	700	48	600	41	490	34	380	26	280	19	170	11		
2315-HLS	3/32	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	960	66		
	1/8	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	900	62	730	50	550	38		
	5/32	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	930	64	810	56	700	48	590	40	470	33	360	25		
	3/16	1000	69	1000	69	1000	69	970	67	890	61	810	56	730	50	650	45	570	39	490	34	410	28	330	23	250	17		
2316-HLS	3/32	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69		
	1/8	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69		
	5/32	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69		
	3/16	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69		
	7/32	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	1000	69	880	61	750	52	620	43		
2413-HLS	1/16	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1420	98	1020	71	630	43		
	5/64	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1460	101	1200	83	940	65	670	47	410	29		
	3/32	1500	103	1500	103	1500	103	1500	103	1500	103	1500	103	1400	97	1220	84	1030	71	850	58	660	46	480	33	290	20		
	7/64	1500	103	1500	103	1500	103	1460	101	1320	91	1180	82	1050	72	910	63	770	53	630	44	490	34	360	25	220	15		
2415-HLS	3/32	1800	124	1800	124	1800	124	1800	124	1800	124	1800	124	1800	124	1800	124	1800	124	1800	124	1560	108	1260	87	960	66		
	1/8	1800	124	1800	124	1800	124	1800	124	1800	124	1780	122	1600	110	1430	98	1250	86	1080	74	900	62	730	50	550	38		
	5/32	1720	119	1610	111	1490	103	1380	95	1270	87	1150	80	1040	72	930	64	810	56	700	48	590	40	470	33	360	25		
	3/16	1210	83	1130	78	1050	72	970	67	890	61	810	56	730	50	650	45	570	39	490	34	410	28	330	23	250	17		
2416-HLS	3/32	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110		
	1/8	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110		
	5/32	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1480	102	1220	84		
	3/16	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1600	110	1580	109	1400	97	1220	84	1040	72	860	59		
	7/32	1600	110	1600	110	1600	110	1600	110	1600	110	1570	108	1440	99	1300	90	1170	81	1040	71	900	62	770	53	640	44		
25133G-HLS	1/16	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	1820	125	1420	98	1020	71	630	43		
	5/64	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	2 120	146	1980	137	1720	119	1460	101	1200	83	940	65	670	47	410	29		
	3/32	2 120	146	2 120	146	2 120	146	1960	135	1770	122	1590	110	1400	97	1220	84	1030	71	850	58	660	46	480	33	290	20		
	7/64	1870	129	1740	120	1600	110	1460	101	1320	91	1180	82	1050	72	910	63	770	53	630	44	490	34	360	25	220	15		
25155G-HLS	5/64	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 210	152	1780	123	1350	93		
	3/32	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 520	174	2 470	170	2 170	150	1870	129	1560	108	1260	87	960	66		
	1/8	2 520	174	2 470	171	2 300	159	2 130	147	1950	135	1780	122	1600	110	1430	98	1250	86	1080	74	900	62	730	50	550	38		
	5/32	1720	119	1610	111	1490	103	1380	95	1270	87	1150	80	1040	72	930	64	810	56	700	48	590	40	470	33	360	25		
	3/16	1210	83	1130	78	1050	72	970	67	890	61	810	56	730	50	650	45	570	39	490	34	410	28	330	23	250	17		
26155G-HLS	5/64	3 700	255	3 700	255	3 700	255	3 700	255	3 700	255	3 700	255	3 700	255	3 490	241	3 060	211	2 630	182	2 210	152	1780	123	1350	93		
	3/32	3 700	255	3 700	255	3 700	255	3 680	254	3 380	233	3 080	212	2 770	191	2 470	170	2 170	150	1870	129	1560	108	1260	87	960	66		
	1/8	2 650	183	2 470	171	2 300	159	2 130	147	1950	135	1780	122	1600	110	1430	98	1250	86	1080	74	900	62	730	50	550	38		
	5/32	1720	119	1610	111	1490	103	1380	95	1270	87	1150	80	1040	72	930	64	810	56	700	48	590	40	470	33	360	25		
3/16	1210	83	1130	78	1050	72	970	67	890	61	810	56	730	50	650	45	570	39	490	34	410	28	330	23	250	17			
Specific Gravity		1.00		.95		.90		.85		.80		.75		.70		.65		.60		.55		.50		.45		.40			

NOTE: If actual specific gravity falls between those shown in above table, use next lower. For example, if actual gravity is 0.73, use 0.70 data.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

High Leverage Spring-Loaded Ball Float Type Drain Traps

For Low Flows at Pressures to 3 700 psig (255 barg) and Specific Gravity Down to 0.40

List of Materials

Table LD-28.					
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
2313-HLS 2315-HLS 2316-HLS	Stainless Steel			ASTM A105 Forged Steel	Compressed Asbestos-free
2413-HLS 2415-HLS 2416-HLS 25133G-HLS 5155G-HLS 6155G-HLS 5155G-HLS 6155G-HLS				ASTM A182 Grade F22 Forged Steel	

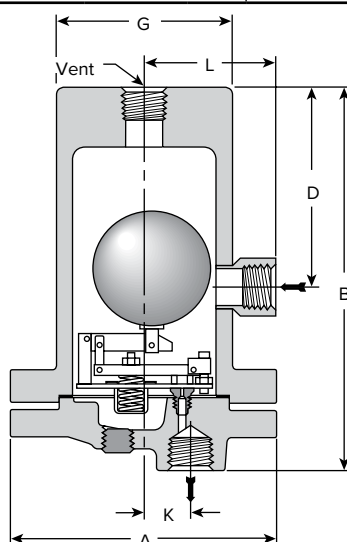


Figure LD-42.

High leverage ball float drain trap.



For a fully detailed certified drawing, refer to CD #1074.

Physical Data

Table LD-29. High Leverage Spring-Loaded Ball Float Type Drain Traps																		
Model No.	2313-HLS†		2315-HLS		2316-HLS		2413-HLS†		2415-HLS†		2416-HLS		25133G-HLS		25155G-HLS		26155G-HLS	
Pipe Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2, 3/4, 1	15, 20, 25	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50	1/2, 3/4, 1	15, 20, 25	1, 1-1/4, 1-1/2	25, 32, 40	1-1/2, 2	40, 50	1/2, 3/4, 1	15, 20, 25	3/4, 1, 1-1/4	20, 25, 32	1, 1-1/4, 1-1/2	25, 32, 40
"A"	8	203	9-3/4	248	11-7/8	302	8-5/8	219	10-3/4	273	12-1/2	318	8-1/2	216	10-3/8	263	11-3/4	298
"B"	11-9/16	294	15-1/16	383	17-1/8	435	11-7/8	3 002	15	381	17-3/4	451	14-1/4	362	16-7/32	412	24-1/8	613
"D"	6-1/16	154	7-13/16	198	9	229	5-3/8	137	7-1/4	184	9	229	3	75	4	102	5	127
"G"	5-1/8	130	6-7/8	175	8-3/8	213	5-3/8	137	6-7/8	175	8-5/8	219	5-3/4	146	7-3/8	187	8-3/8	213
"K"	1-7/16	37	1-3/4	44	2-1/8	54	1-7/16	37	1-3/4	44	2-1/8	54	1-5/16	33	1-3/4	44	1-3/4	44
"L"	3-7/8	98	4-11/16	119	5-3/4	146	4	102	4-13/16	122	5-13/16	148	—	—	—	—	—	—
Weight, lbs (kg)	46 (21)		98 (44)		160 (73)		69 (31)		130 (59)		210 (95)		113 (51)		171 (78)		325 (147)	
Maximum Allowable Pressure (Vessel Design)	1 000 psig @ 100°F (69 barg @ 38°C) 600 psig @ 750°F (41 barg @ 400°C)						1 500 psig @ 100°F (103 barg @ 38°C) 900 psig @ 850°F (62 barg @ 454°C)		1 800 psig @ 100°F (125 barg @ 38°C) 900 psig @ 900°F (62 barg @ 482°C)				2 120 psig @ 100°F (146 barg @ 38°C) 1 700 psig @ 900°F (117 barg @ 482°C)		2 520 psig @ 100°F (174 barg @ 38°C) 2 000 psig @ 900°F (138 barg @ 482°C)		3 700 psig @ 100°F (255 barg @ 38°C) 3 000 psig @ 900°F (207 barg @ 482°C)	

Note: Available with screwed, socketweld or flanged connections.

† Available with cast 316 stainless steel body and all stainless steel internals. Consult factory.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.



Free Floating Lever Dual Gravity Drain Traps

For Pressures to 1 000 psig (69 barg)

Armstrong free floating lever dual gravity drain traps are identical to the units described on pages LD-38 and LD-40 except float weights are modified to make them suitable for draining water from a light liquid. If you wish to use them for draining any liquid with specific gravity other than 1.00, consult the Armstrong Application Engineering Department.

Floats for dual gravity drain traps are weighted with quenching oil which, in the unlikely possibility of float failure, may be dispersed through the system. If this is a hazard, consult the Armstrong Application Engineering Department.

NOTE: Armstrong can design dual gravity traps for venting light liquids from above heavier liquids. Consult the Armstrong Application Engineering Department.

Viscosity Considerations for Dual Gravity Traps

The operation of dual gravity traps depends upon a float that will sink in the light liquid and float in the heavy liquid. When the specific gravities of the two liquids are very close, the available operating forces are, therefore, also very small. Viscous fluids may impair the ability of the trap to respond to changing liquid levels.

Consult Armstrong's Application Engineering Department if your application involves fluids more viscous than 70 cs, which is approximately the viscosity of a light machine oil.

Table LD-30. Maximum Operating Pressures for Draining Water From Different Specific Gravity Liquids With Orifices Available in Dual Gravity Drain Traps (See pages LD-29 and LD-30.)

Model No.	Sp. Grav.	.50		.55		.60		.65		.70		.75		.80		.85		
	Float Wt, oz	6.0		6.5		7.0		7.5		8.0		8.5		9.1		9.6		
	Float Wt, g	170		184		199		213		228		242		257		271		
	Orifice (in)	Maximum Operating Pressure																
		psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	
2-DG	5/16	15	1.0	12	0.9	10	0.7	9	0.6	7	0.5	5	0.35	—	—	—	—	
	1/4	25	1.6	20	1.4	18	1.2	15	1.0	12	0.8	9	0.6	6	0.4	—	—	
	3/16	50	3.6	45	3.0	40	2.6	30	2.2	25	1.8	20	1.4	12	0.9	7	0.45	
	5/32	90	6.0	75	5.5	65	4.6	55	3.8	45	3.0	35	2.4	22	1.6	12	0.8	
	1/8	150	10	130	9.0	110	8.0	90	6.5	75	5.0	55	4.0	40	2.6	20	1.4	
	7/64	190	13	170	12	150	10	120	8.5	100	6.5	75	5.0	50	3.4	25	1.8	
32-DG	Sp. Grav.	.50		.55		.60		.65		.70		.75		.80		.85		
	Float Wt, oz	8.8		9.6		10.3		11.1		11.9		12.7		13.5		14.3		
	Float Wt, g	248		271		293		315		338		360		382		405		
	Orifice (in)	Maximum Operating Pressure																
	5/16	25	1.6	20	1.4	18	1.2	15	1.0	12	0.9	10	0.7	7	0.5	—	—	
	1/4	40	2.6	35	2.4	30	2.0	25	1.8	22	1.4	18	1.2	12	0.8	8	0.5	
	3/16	90	6.0	75	5.0	65	4.6	55	3.8	45	3.2	35	2.6	25	1.8	18	1.2	
	5/32	150	10	130	9.0	110	8.0	100	6.5	80	5.5	65	4.4	45	3.2	30	2.0	
	1/8	250	17	225	15	200	13	170	11	140	9.5	110	7.5	80	5.5	50	3.4	
7/64	325	22	275	20	250	17	225	15	180	12	140	9.5	100	7.0	65	4.4		
3-DG to 250 psig* (17 barg) Cast Iron 33-DG for all pressures	Sp. Grav.	.50		.55		.60		.65		.70		.75		.80		.85		
	Float Wt, oz	11.2		12.2		13.2		14.2		15.2		16.1		17.1		18.1		
	Float Wt, g	317		345		373		401		430		458		486		514		
	Orifice (in)	Maximum Operating Pressure																
	1/2	12	0.8	10	0.7	9	0.6	8	0.5	6	0.45	5	0.35	—	—	—	—	
	3/8	25	1.8	22	1.6	20	1.4	15	1.2	12	0.9	10	0.7	7	0.5	—	—	
	5/16	40	2.8	35	2.4	30	2.2	25	1.8	22	1.4	15	1.2	12	0.8	7	0.5	
	9/32	55	3.6	45	3.2	40	2.8	35	2.4	30	2.0	22	1.6	15	1.0	9	0.6	
	1/4	80	5.5	70	4.8	60	4.2	50	3.6	40	3.0	35	2.2	25	1.6	15	1.0	
	7/32	110	8.0	100	7.0	90	6.0	75	5.0	60	4.2	45	3.2	35	2.4	20	1.4	
	3/16	170	12	150	10	130	9.0	110	7.5	90	6.5	70	4.8	50	3.4	30	2.0	
	5/32	275	19	225	16	200	14	170	12	140	10	110	7.5	80	5.5	45	3.2	
1/8	550	38	475	34	425	28	350	24	300	20	225	15	160	11	100	6.5		
7/64	700	48	600	42	525	36	450	32	375	26	275	20	200	14	120	8.5		
6-DG to 250 psig* (17 barg) Cast Iron 36-DG to 1 000 psig (69 barg) Steel	Sp. Grav.	.50		.55		.60		.65		.70		.75		.80		.85		
	Float Wt, oz	52		57		62		67		72		77		82		87		
	Float Wt, g	1 483		1 622		1 760		1 899		2 038		2 177		2 316		2 455		
	Orifice (in)	Maximum Operating Pressure																
	1-1/16	12	0.9	12	0.8	10	0.7	9	0.6	8	0.5	6	0.4	—	—	—	—	
	7/8	22	1.4	18	1.2	18	1.2	15	1.0	12	0.8	10	0.7	7	0.5	5	0.35	
	3/4	30	2.2	25	1.8	25	1.6	20	1.4	18	1.2	15	1.0	10	0.7	7	0.5	
	5/8	45	3.2	40	2.8	35	2.6	30	2.2	25	1.8	22	1.4	15	1.2	12	0.8	
	9/16	60	4.2	55	3.8	50	3.4	40	2.8	35	2.4	30	2.0	22	1.4	15	1.0	
	1/2	90	6.0	80	5.5	70	4.8	60	4.2	50	3.4	40	2.8	30	2.2	22	1.4	
	7/16	130	9.0	110	8.0	100	7.0	90	6.0	70	5.0	60	4.0	45	3.0	30	2.0	
	3/8	200	14	180	12	160	11	140	9.5	110	8.0	90	6.5	70	4.8	50	3.2	
	11/32	275	18	250	16	200	14	180	12	150	10	120	8.5	90	6.5	65	4.4	
	5/16	350	24	300	22	275	19	225	16	190	13	160	11	120	8.0	80	5.5	
	9/32	450	32	400	28	350	24	300	20	250	18	200	14	160	11	110	7.5	
	1/4	650	46	575	40	525	36	450	30	375	26	300	20	225	16	160	11	
	7/32	950	65	850	55	750	50	650	44	525	36	425	30	325	22	225	15	
	3/16	1 000	69	1 000	69	1 000	69	1 000	69	850	60	700	48	525	36	350	24	

NOTE: If actual specific gravity falls between those shown in the above table, use the next higher gravity. For example, if actual gravity is 0.73, use 0.75 gravity data.
*For vessel pressures above 250 psig (17 barg), always use steel drain traps.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Free Floating Lever Dual Gravity Drain Traps

For Pressures to 1 000 psig (69 barg)

List of Materials

Table LD-31.					
Model No.	Valve & Seat	Leverage System	Float	Body & Cap	Gasket
2-DG 3-DG 6-DG	Stainless Steel			Cast Iron ASTM A48 Class 30	Compressed Asbestos-free
32-DG 33-DG 36-DG				Forged Steel ASTM A105	

For information on special materials, consult the Armstrong Application Engineering Department.

For a fully detailed certified drawing, refer to:

No. 2-DG, 3-DG, 6-DG **CD #1034**

No. 32-DG, 33-DG, 36-DG **CD #1035**

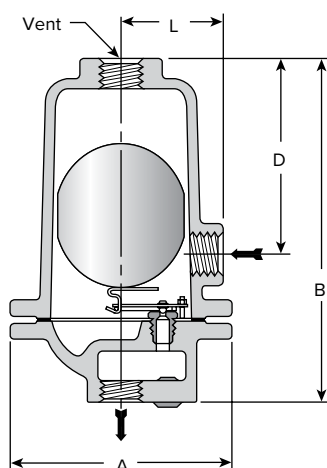


Figure LD-43.

No. 2-DG, 3-DG and 6-DG cast iron dual gravity drain traps.

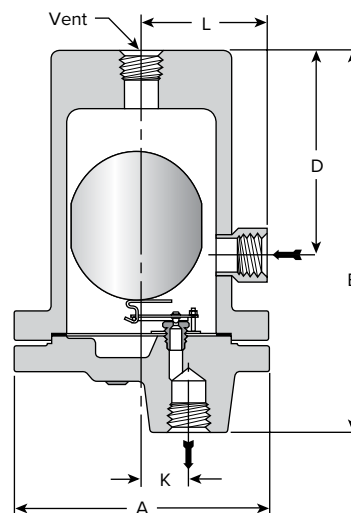


Figure LD-44.

No. 32-DG, 33-DG and 36-DG Forged steel dual gravity drain traps. Socketweld or flanged connections are also available.

Physical Data

Table LD-32. Armstrong Free Floating Lever Dual Gravity Drain Traps												
Model No.	Cast Iron						Forged Steel					
	2-DG		3-DG		6-DG		32-DG*		33-DG*		36-DG*	
Pipe Connections	in	mm	in	mm	in	mm	in	mm	in	mm	in	mm
	1/2, 3/4	15, 20	1/2, 3/4, 1	15, 20, 25	1-1/2, 2	40, 50	1/2, 3/4, 1	15, 20, 25	1/2, 3/4, 1	15, 20, 25	1-1/2, 2	40, 50
"A"	5-1/4	133	6-3/8	161	10-3/16	259	6-3/4	171	8	203	11-7/8	302
"B"	8-3/4	222	11-1/2	292	18	457	10-3/16	259	11-9/16	297	17-1/8	435
"D"	5-1/8	103	7	188	9-3/8	238	5-9/16	141	6-1/16	154	9	229
"K"	—	—	—	—	—	—	1-1/4	32	1-7/16	37	2-1/8	54
"L"	2-7/16	62	2-7/8	73	4-5/8	117	3-3/8	86	3-7/8	98	6-1/16	154
Approx. Wt. lbs (kg)	12 (5.5)		21 (9.5)		78 (35.5)		31 (14)		49 (22)		163 (74)	
Maximum Allowable Pressure (Vessel Design)	250 psig @ 450°F (17 barg @ 232°C)						600 psig @ 100°F (41 barg @ 38°C) 500 psig @ 750°F (35 barg @ 400°C)		1 000 psig @ 100°F (69 barg @ 38°C) 600 psig @ 750°F (41 barg @ 400°C)			

* Available in Type 316 stainless steel. Consult factory.

Designs, materials, weights and performance ratings are approximate and subject to change without notice. Visit armstronginternational.com for up-to-date information.

Armstrong ultra-capacity ball float drain traps are designed to meet exceptionally large capacity needs in draining water and other liquids from air or other gases under pressure.

425°F (17 barg @ 218°C). When ordering, be sure to specify "Liquid Drainer" or "LD." Example, LS-series LD, 2" (50 mm) NPT, 7/8" orifice.

Options. L and M Series drain traps are available with armored gauge glass with a maximum allowable pressure of 250 psig @

For a fully detailed certified drawing, refer to:
L and M Series, CD #1010 JD and KD Series, CD #1302

Table LD-33. Maximum Operating Pressures for Handling Different Specific Gravity Liquids With Orifices Available in Ultra-Capacity Drain Traps

Model No.	Specific Gravity	1.00		.95		.90		.85		.80		.75		.70		.65		.60		.55		.50	
	Orifice Size	Maximum Operating Pressure																					
	in	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg	psig	barg
JD	1-1/16	16	1.0	15	1.0	13	0.89	12	0.82	11	0.75	10	0.69	9	0.62	7	0.48	6	0.41	5	0.34	4	0.28
	3/4	35	2.4	32	2.2	30	2.0	27	1.8	24	1.6	22	1.5	19	1.3	16	1.0	14	0.97	11	0.75	9	0.62
	9/16	87	6.0	81	5.5	75	5.0	68	4.6	61	4.2	55	3.8	48	3.3	41	2.8	35	2.4	28	1.8	22	1.5
	1/2	146	10	135	9.0	125	8.5	113	8.0	102	7.0	91	6.2	81	5.5	69	4.8	59	4.0	47	3.2	37	2.6
	7/16	175	12	175	12	175	12	175	12	158	11	141	10	125	8.5	107	7.3	91	6.2	73	5.0	57	3.9
	3/8	250	17	232	16	214	15	195	13	177	12.2	159	10.9	140	9.7	122	8.4	103	7.1	85	5.9	67	4.6
	5/16	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	300	20.6	279	19.2	219	15.0
30KD	1-7/8 dual orifice	30	2	30	2	30	2	30	2	—	—	—	—	—	—	—	—	—	—	—	—	—	—
50KD		50	3.5	50	3.5	50	3.5	50	3.5	—	—	—	—	—	—	—	—	—	—	—	—	—	
300KD		300	21	300	21	300	21	300	21	—	—	—	—	—	—	—	—	—	—	—	—	—	
L to 250 psig (17 barg)	1-5/8	35	2.4	32	2.2	30	2.0	27	1.8	25	1.6	23	1.6	20	1.4	18	1.2	15	1.0	13	0.89	10	0.69
	1-1/8	116	8.0	108	7.4	100	7.0	92	6.3	84	5.8	76	5.2	68	4.7	60	4.1	52	3.6	44	3.0	36	2.5
	7/8	174	12	162	11	150	10.5	138	9.5	126	8.6	114	7.9	102	7.0	90	6.2	78	5.4	65	4.5	53	3.7
	11/16	*315	*22	*294	*20	*272	*19	250	17	228	16	206	14	184	13	162	11	141	9.7	119	8.2	97	6.7
	For all Pressures	1/2	*450	*31	*450	*31	*450	*31	*450	*31	*450	*31	*400	*28	*354	*24	*298	*21	248	17	197	14	147
M to 250 psig (17 barg)	1-7/8 dual orifice	250	17	250	17	250	17	250	17	—	—	—	—	—	—	—	—	—	—	—	—	—	—
	1-17/32 dual orifice	*450	*31	*450	*31	*450	*31	*450	*31	*450	*31	—	—	—	—	—	—	—	—	—	—	—	—
MS For all Pressures																							

*These pressures applicable only to LS and MS models.

List of Materials

Table LD-34.

Name of Part		Material	
		Series JD, KD, L & M	Series LS & MS
Cap & Body	JD, KD	ASTM A395 Ductile Iron	ASTM A216 Grade WCB
	L, M	ASTM A48 Class 31	
Cap	L, LS	304 Stainless Steel, ASTM A351 Grade CF8	
Extension*	KD, M, MS	17-4 Ph, ASTM A747 Grade CB7Cu-1	
Cap Bolting		ASTM A193 Grade B 7**	ASTM A193 Grade B 7
Cap Gaskets		Flexible Graphite	
Float Mechanism		Stainless Steel	

* JD Series does not have cap extension.

**JD and KD Series - ASTM A307 Grade B.

Physical Data

Table LD-36. Ultra-Capacity Drain Traps

Trap Series	JD & KD		L & M		LS & MS	
	in	mm	in	mm	in	mm
"B"	13-1/16	332	20-1/4	514	20	508
"C"	9-5/8	244	14-3/4	375	15-1/4	387
"H"	13-7/8	352	19-3/4	502	20	508
"M"	6-1/2	165	11-5/16	287	11-5/16	287
"D"	3	76	4-3/16	106	4-3/16	106
"S"	—	—	3-3/4	95	3-3/4	95
"T"	—	—	12	305	12	305
Weight lbs (kg)	100 (45)		196 (89)		290 (132)	
Max. Allow. Pressure (Vessel Design)	300 psig @ 650°F (21 barg @ 343°C)		250 psig @ 450°F (17 barg @ 232°C)		450 psig @ 650°F (31 barg @ 338°C)	

JD, KD, L and M Series also may be used for steam service as float and thermostatic traps and as condensate controllers. Steam service capacities for all configurations are given in the Steam Trapping section of this catalog.

Connections Available

Table LD-35.

Model	Size		NPT	BSPT	SW	FLG
	in	mm				
JD	2	50	X	X	—	*
KD	2, 2-1/2, 3	50, 65, 80	X	X	—	*
L	2, 2-1/2	50, 65	X	X	—	X
M	3	80	X	X	—	X
LS	2, 2-1/2	50, 65	X	X	X	X
MS	3	80	X	X	X	X

*Flanged connections available. Consult factory.

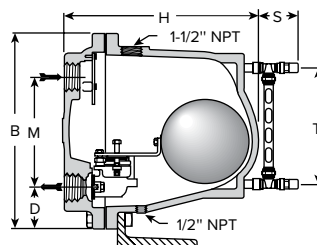


Figure LD-45.
L and LS Series

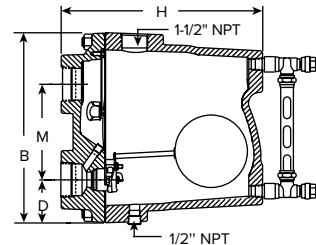


Figure LD-46.
JD and KD Series

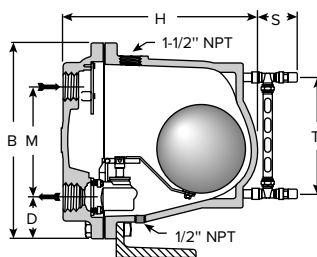
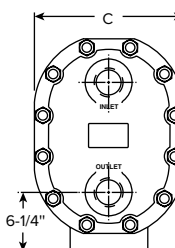


Figure LD-47.
M and MS Series



Installation and Maintenance of Drain Traps

For Draining Liquid From Gas...for Draining Water From Light Liquid

Installation Procedures

Pipe Fitting. Adhere to good piping practice. Clean pipes carefully after cutting and threading before hooking up traps. Before connecting traps to system, blow down at full pressure to clear the pipes of dirt, pipe cuttings and other foreign objects.

Strainers are necessary if there is a chance scale and sediment can be carried to the trap.

Blowdown Valves may prove useful.

Shutoff Valves & Unions should be provided so the drain trap can be examined and/or serviced without shutting down the unit drained.

Operation. Maximum operating pressure is stamped on the trap. Do not exceed this pressure.

- A.** Ball float drain traps must be located below the drain point.
- B.** Make inlet piping as short as possible with a minimum of elbows and other restrictions.
- C.** Back venting usually required on ball float drain traps.
 1. Pressure vessels should be vented back to any convenient point above the liquid level. Use a full-ported valve in the back-vent line. On larger traps (6 and 36-LD and larger) use a minimum of 3/4" (20 mm) nominal pipe for back venting—1" (25 mm) or larger preferred for heavy loads. Remember, the pressure in the unit drained and in the drain trap are the same—only the difference in liquid levels produces flow.
 2. Separators and drip points should be vented to the downstream side of the unit.
 3. On very light loads, venting is not necessary, but use at least a 3/4" (20 mm) connection between the vessel and the trap. Make sure inlet line is vertical or pitched to trap.
 4. Float type drain traps do not require priming.

Typical installations of drain traps are shown in drawings in "Installation and Maintenance of Drain Traps" section.

Drain Trap Testing and Troubleshooting

Testing Schedule

A regular schedule should be set up for testing and preventive maintenance. Size and operating pressure determine how frequently drain traps should be checked. Units on normal industrial applications should be checked as follows:

High Pressure Drain Traps—250 psig (17 barg) and up. Test daily to weekly.

Medium Pressure Drain Traps—60 to 250 psig (4 to 17 barg). Test weekly to monthly.

Low Pressure Drain Traps—1 to 60 psig (0.07 to 4 barg). Test monthly to annually. Large traps on high capacity jobs can be tested more frequently to good advantage.

Drain Traps on gas and other critical applications should be checked at the same time valves and other line equipment are inspected. Your own experience will determine the required testing schedule.

Troubleshooting

- A.** Drain trap does not discharge.
 1. Insufficient liquid coming to drain trap to permit discharge. Continue operation.
 2. Drain trap filled with dirt or sludge. Remove cap and mechanism; clean thoroughly. Install strainer in inlet side of drain trap.
 3. Differential pressure across drain trap too high. Check inlet and outlet pressure. If the difference exceeds the maximum operating pressure stamped on the drain trap, the valve will remain closed. Reduce differential pressure if possible, or install properly sized mechanism in drain trap if possible.
 4. Worn valve seat. As the seat becomes worn, the seating surface area enlarges, lowering the trap's maximum operating pressure. Replace with new parts.
 5. Inlet or outlet line valves closed. Open valves.
 6. Strainer clogged. Clean strainer screen.
 7. Float defective or collapsed. Replace float.
- B.** Drain trap discharges continuously.
 1. If drain trap discharges full stream of liquid continuously and vessel fills full of liquid—
 - a. Drain trap too small for job. Replace with correct size.
 - b. Abnormal amounts of liquid coming to drain trap. Remedy cause or replace with drain trap that has a larger capacity and will handle peak loads.
- C.** Drain trap blows through.
 1. Dirt or scale on valve or seat. Remove cap, clean drain trap, as well as valve and seat.
 2. Worn valve, or seat that is wire-drawn. Remove cap, replace mechanism.
 3. IB trap may lose its prime.
 - a. Close the inlet valve for a few minutes. Then gradually open. If the drain trap catches its prime, the chances are that the trap is all right.
 - b. Frequent loss of prime may require an internal check valve or, if trap is old, valve and seat may be worn.

In the event of any unusual maintenance or operational difficulty, consult your Armstrong Representative, or the Armstrong International Application Engineering Department.

Installation of Armstrong drain traps for the most satisfactory operation requires that a few simple rules be observed:

Clean Piping. First install piping and valve ahead of trap, then blow down at full air pressure to remove loose dirt. Last of all, screw the trap into position.

Location. Compressed drain traps should be located below and close to the unit being drained (See Figs. LD-48 and LD-50), or as directed by the equipment manufacturer. When headroom is inadequate, inverted bucket drain traps can be installed above the unit drained, but they must be equipped with a check valve in the inlet line (See Fig. LD-49). They should be accessible for maintenance.

Priming. Prime bodies of inverted bucket drain traps before turning on the air. Ball float traps do not require priming.

Back Venting (Ball Float Traps Only). Ordinarily a drain trap has little water to handle, and a single line to the *top of the trap* is sufficient. However, if a ball float trap must be installed at some distance from the drip point, or if there are large quantities of water to be discharged, back venting is good insurance for positive and fast flow of water to the drain (See Fig. LD-52). Be sure there are no pockets in the vent line in which water could collect and prevent venting (See Fig. LD-54). If high water level is objectionable, raise the receiver, or dig a pit so top of trap can be at the same level as the bottom of the drain line (See Fig. LD-53). Otherwise, use an inverted bucket trap that can be installed above the drip point (See Fig. LD-49).

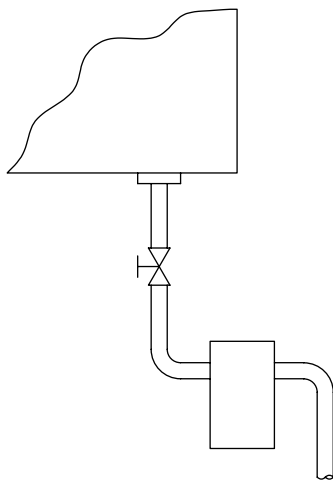


Figure LD-48.
Standard hookup for inverted bucket drain trap BVS. **Be sure to fill trap body with water before opening the valve.**

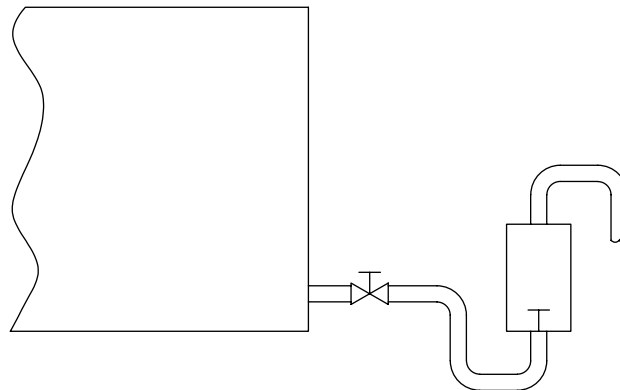


Figure LD-49.
The inverted bucket trap draining an air receiver where space limitations prevent installation below the receiver. Note trap should either have internal check valve or a swing check to prevent prime loss when air pressure drops.

Installation and Maintenance of Drain Traps

For Draining Liquid From Gas...for Draining Water From Light Liquid

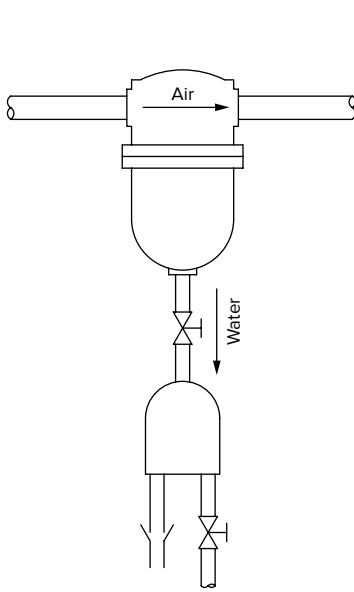


Figure LD-50.

Drain trap installed below an air line separator. Keep the pipe as short as possible.

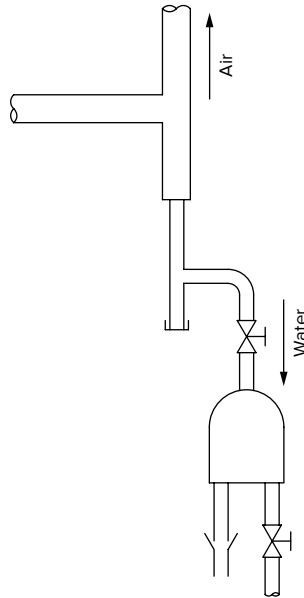


Figure LD-51.

Drain trap draining air line drip pocket. Be sure to use a gate valve and blow down the assembly before installing trap.

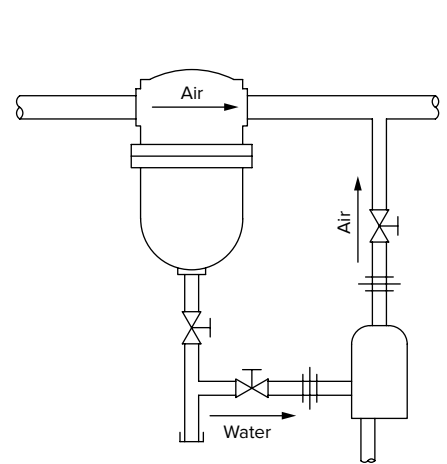


Figure LD-52.

Drain trap with vent line to downstream side of air separator to assure positive and fast flow of water to the trap. Note side inlet connection from separator.

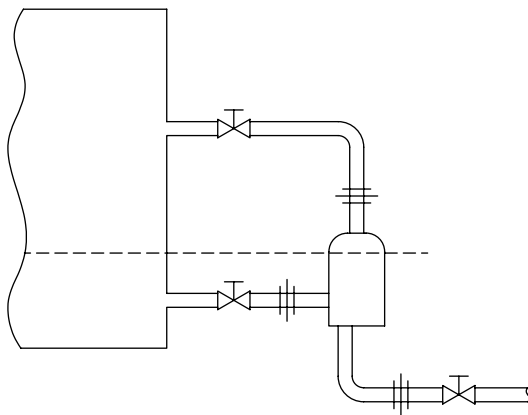


Figure LD-53.

Drain trap installed at side of receiver, close to floor. Water will rise to broken line before trap opens.

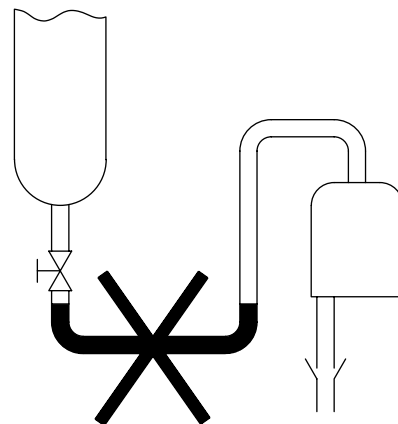


Figure LD-54.

Do not install a ball float trap above the drip point or put a loop or pocket in the line to the trap. The water seal prevents air from leaving trap body and allowing liquid to enter.